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MESN99-020-OA Page 1

New Technologies Engineering Division

Mechanical Engineering Safety Note

Time Projection Chamber

MESN99-020-OA

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Contents

А.	Description	3
B.	Operational Hazards	5
C.	Procedures	5
D.	Calculations	5
	Vessel	6
	Head / Flange Calculations	7
	Fracture Critical Components	11
	Fragment Hazard Mitigation	12
E.	Testing Requirements	13
F.	Labeling Requirements	13
G.	Associated Procedures	15
H.	References and Notes	15
APPEN	IDIX A: PROOF TESTING PROCEDURE FOR THE TPC	16
APPEN	IDIX B DRAWINGS	20
APPEN	IDIX C CALCULATIONS	

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A. Description

This safety note covers the design of time projection chambers (TPC) used in a full volume imaging detector. The chambers are used in building 132N, room 2723. There are three parts to the full volume imaging detector system. The first part is the gas purification subsystem that is used to purify and deliver electronegative free (99.9999999%) gas. This part of the system is being built commercially by Insync Systems. The second part of the system, designed and built at LLNL, includes the time projection chambers (TPC) where the experiments will be performed. Gas, from the purification panel, feeds the TPC's that will nominally operate at 300 psig but are being designed for 350 psig maximum operating pressure (MOP). It will be necessary to work around the TPC's with radioactive sealed sources for testing and calibration; thus this is a manned operation. The third part of the system uses cylinders to reclaim the purified gas. These cylinders have been fabricated by ACME CRYOGENICS INC. and are rated by them at 3000 psig MAWP. Gas will be transferred in the TPC system by thermal cycles, using LN2 to create the temperature gradient inside the chamber via conduction through the walls of the cryogenic thimble. A certain percentage of alcohol may be used in the LN2 bath to move the temperature of the bath above 73K.

The TPC's are the experimental chambers designed at LLNL. These chambers are used for two purposes but were mechanically designed to be identical. The first chamber will be used as an ionization chamber where electron drift will be used as a measure of gas purity. The second chamber is the actual TPC itself, which is used for position sensitive readout of electron clouds and hence gamma ray imaging. Figure 1 depicts a TPC with its associated hardware. In the experimental setup, the chambers are connected together with high pressure tubing. The chambers have been designed to allow a 400 keV gamma ray to penetrate the chamber wall in well-defined places, specifically in the center of the 2 3/4 inch conflat flange and in a linear series of VCR blanks on the side of the chamber. It will be necessary to use radioactive sources in conjunction with these windows to probe the capabilities of the chamber. The 1 3/4 inch conflat flanges has been outfitted with a high voltage (20 kV) ceramic feedthrough from Ceramaseal. Many of the penetrations into the chamber and the internals of the chamber are attached to the conflat gasketed chamber head to allow easy removal from the chamber body. The chambers will be filled with a gas (Ar, Xe, along with at least one the following: CH4, CO2, and P10) using the 135psi gas purification system and then condensed by cooling the chamber using a cryogenic thimble. LN2 will envelope the outside of the thimble creating non-uniform thermal stresses along with membrane stress throughout the vessel.

This ME Safety Note is required because the TPC of the system contains compressed gas at pressures exceeding 150 psig or 100kJ of stored energy. This Safety Note covers the vessel depicted in Figure 1 up to and including the output connections. If required, a separate safety note will cover the remaining parts of full volume imaging detector system less the TCP's.



Figure 1 – Diagram of the Time Projection Chambers (TPC)

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B. Operational Hazards

Associated hazards are those typical of any high pressure gas system. Failure of a vessel or component could result in either shrapnel or a blast overpressure to the body. Since the gases involved are not air, there is also the potential concern of asphyxiation. Other hazards include physical exposure to the radioactive sealed source and cold temperatures. The hazards other than those associated with the pressure vessel will be addressed by the FSP (if applicable) or separate OSP for this experiment.

C. Procedures

Design safety factors are robust for all intended pressures. The system is adequately protected by a pressure relief device at a VCR port so that components cannot be over-pressurized. This document also specifies shielding requirements for personnel protection from shrapnel in the event of an accident. However, an OSP for this experiment will address associated interlocks and operational steps required during pressurization.

D. Calculations

The following will certify the TPC for this system:

[1] Hardware and Fabrication

The vessel is fabricated using commercially purchased metals. Fabrication and joining techniques are also standard technology. Welding was performed by LLNL ASME certified welders experienced in pressure systems.

[2] Engineered Design

The system design has relief devices at strategic locations (a VCR fitting) to insure that the MAWP's are never exceeded.

An evaluation of high risk pressure components indicated that a Ceramaseal feedthrough may fail if improperly handled. Specifically, the weld joint at the Conflat is susceptible to bending and fracture. To minimize this risk, a fragment deflector/stop fixture was designed and will be mounted in front of the head where the Ceramaseal is mounted. A Kevlar drape will also be employed if this device fails to capture all fragments. This stop and Kevlar drape will be interlocked during pressure vessel operation.

[3] <u>Testing</u>

Detailed proof testing procedures at 1.5 times MAWP and at the working temperature, induced by LN2 cooling, have been developed and are enclosed as Appendix A. Successful completion of these procedures by a LLNL pressure inspector will complete the certification of the TPC's. Proof testing is the crux of pressure vessel qualification for fracture critical components and is best stated from literature⁵ as follows:

"The critical flaw size associated with proof test conditions can also be used for life expectance considerations. Specifically, if a pressure vessel survives a given proof test it can be concluded that the largest defect present in the structure is smaller than the critical flaw size at the proof test conditions. Therefore, in the absence of non-destructive inspection, this flaw size can be considered the existing flaw size at the beginning of life at the operating conditions and would, in turn, serve as the basis for further crack growth consideration"⁵ (also see fracture analysis below).

The vessel has been designed to meet ASME Boiler and Pressure Vessel Code design guidelines. Stresses are low enough to eliminate the need for impact testing of the material in the heat effected zones created by the butt welds, UHA-51 (g) (see misc.nb calculations in Appendix C). The ASME Code also exempt austenitic, chromium-nickel stainless steels from impact testing, UHA-51(d)(1)(a). Thus, the base materials 304L and 316L are exempt.

[4] <u>Calculations</u>

Most calculations were done using ASME Pressure Vessel Code, Section VIII, Division 1 guidelines. The TPC has a MAWP of 978 psig when using the C-Ring type head (no openings) and 402 psig for the Conflat type head(s) (with and without openings). A future addendum to this safety note will cover a head (with openings) to be used at 978 psig MAWP. The allowable stresses used in all calculations are based on values found in the ASME Pressure Vessel Code, Section II. For both 316L and 304L the allowable stress is 16,700 psi which provides a nominal Safety Factor of ~5 in all Pressure Vessel Code calculations (i.e., head thickness, maximum vessel pressure, minimum wall thickness, etc). The following tables are summaries of the detailed calculations found in Appendix A.

Vessel

The energy in each pressure vessel was calculated to be 55, 852 ft-lb. or 16.4 g TNT at the MAWP of 978 psig. The following table summarizes the analytical results for the main 8 inch schedule 80 pressure vessel, the detector pipe, the VCR "Cajon" fittings/ pipes, and the LN₂ pipe connected to the main vessel. All tubing is 316L. Calculations were made at a MAWP of 978 psig. The last column refers to the ratio of yield stress (37ksi) to Von Mises stress at the test pressure of 1.5 x MAWP. Values must be greater than 1.0 for a safe proof test.

	S1 (psi)	S2 (psi)	S3 (psi)	Von Mises (psi)	Required wall thickness (in)	Actual wall thickness (in)	If ≥ 1.0 stress less than yield for 1.5xMA WP
Main 8" vessel	3499	7976	-978	7755	0.336	0.500	3.2
Detector pipe 2.87 OD	1839	4657	-978	4880	0.102	0.275	5.1

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VCR pipe 0.5" OD	1739	4455	-978	4705	0.012	0.050	5.2
LN2 pipe 1.9" OD	1618	4214	-978	4496	0.066	0.200	5.5

Analytical results for welds, area reinforcement, and their related loads that attach the detector pipe, LN_2 pipe, and VCR pipe to the main vessel shell are detailed in the table below at a MAWP of 978 psig. Generally, if the nozzle and fillet weld load paths are greater than the total weld load, then the strengths are sufficient. The total weld load (W~(Area required – Area available)*Allowable stress)) for the VCR pipe is less than 0 because the vessel wall is 0.160" thicker than required creating much more area available than required. Thus, the area available is greater than the area removed and a negative number results.

	Area of mat'l. required (in^2)	Area of mat'l. avail. (in^2)	Total weld load (lb)	Nozzle wall load path (lb)	Fillet weld load path (lb)
Detector pipe	0.780	0.800	8172	13172	12749
LN ₂ pipe	0.504	0.508	5396	6243	6106
VCR pipe	0.134	0.194	< 0	413	402

The butt welds connecting the hub to the main vessel and the ellipsiodal head to the main vessel, the ellipsiodal head on liquid nitrogen pipe, and the hub to the detector pipe, reduced the allowable working pressure in the vessel they are connected to by 'E' (butt weld efficiency). An 'E' of 0.7 was used for these welds which reduced their associated allowable working pressures to 1421 psig, 6979 psig, and 6139 psig for the of the main vessel, LN pipe, and detector pipe respectively. Again, all of these calculated pressures use an allowable stress of 16,700 psi which has a nominal SF = 5.0 so an additional SF of 1.5 (1421 / 978) is obtained. Using a butt weld efficiency of 0.7 allows no radiography to be performed on the welds according to the ASME Boiler and Pressure Codes.

The VCR, LN_2 , and detector port openings in the vessel shell are mounted 90° to each other. The radial distance between hole centers is approximately 6.0 inches. ASME Boiler Code requires that all openings be less than the sum of their respective diameters. The maximum sum of the diameters is 3.37 inches between LN_2 and the detector port.

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Holes that do not penetrate the vessel shell may be required to horizontally mount the vessel. The depth of tapped 1/4-20 holes and 3/8-16 holes shall be ≤ 0.25 inches. Holes can not be placed near other openings or reinforcements.

Head / Flange Calculations

The following table summarizes the analytical results for the integral flange butt welded to the main access port and the small flange butt welded on the side of the

Flange	MOP	Longitudi nal hub stress (psi)	Radial flange stress (psi)	Tangential flange stress (psi)
Main 10.5" OD	850	16973	6327	4173
Main 10.5" OD	350	6388	2381	1571
Detector 4.625" OD	850	13998	2794	7367

vessel (detector port). Again, the allowable stress in 16,700 psi for the base material. Also, the ASME allowable hub stress is 1.5 time the allowable stress.

The head for operating at 850 psig, uses a C-Ring type metal seal and is made from 304L stainless steel. The (24) required bolts for this flange are Unbrako KS 1216 1/2"-13 SHCS with a tensile strength of 160,000 psi (or 304 Stainless Steel with a 81 ksi tensile strength). The main flange for operating at 350 psig is a Conflat (CF) type (304L), sealed with a soft copper flat gasket to a knife edge. The (24) required bolts for this flange are Unbrako KS 1216 1/2"-13 SHCS with a tensile strength of 160,000 psi (or 304 Stainless Steel with a 81 ksi tensile strength). All other CF flanges (1 1/3 and 2 3/4 inch) shall be bolted to the 350 MOP head using Unbrako KS 1216 psi (or 304 Stainless Steel with a 81 ksi tensile strength), 8-32 or 1/4-28 SHCS as required.

The smaller 4 5/8" CF type flange for the detector port requires 10 bolts, Unbrako KS 1216 5/16"-24 SHCS with a tensile strength of 160,000 psi (or 304 Stainless Steel with a 81 ksi tensile strength) and is made from 304L stainless steel. The following table summarizes the fastener calculations.

Flange	MOP	No. of bolts	Bolt	Torqu e (in- lb)	Flange design bolt load, operating. (lb)	Flange design bolt load, gasket seal. (lb)	Max. allowable bolt load (SF 4 applied)
Main, C-ring 10.5" OD	850	24	1/2-13	1140	58850	96913	134976
Main, CF 10.5" OD	350	24	1/2-13	1140	24677	79827	134976
Detector 4.625" OD	850	10	5/16- 24	347	10144	15452	20760
1 1/3" CF	350	6	#8-32	51	231	230	2936
2 3/4" CF	350	6	1/4-28	152	1015	527	7937

Analytical results for the commercially purchased SA316 ellipsiodal head on main vessel, nominal wall thickness 0.5 inches and the SA316 ellipsiodal head on liquid nitrogen pipe, nominal wall thickness 0.2 inches follows. The head

	MOP	Max. pressure (psig)	Required head thickness (in)	Actual head thickness (in)	If \geq 1.0 stress less than yield for 1.5x MAWP
Main vessel	850	1513	0.320	0.500	1.03
LN ₂ pipe	850	3036	0.063	0.200	2.07

thickness calculations were done at the MAWP of 978 psig and allow for strength reduction due to the butt weld connecting them to the vessel.

Results of the unstayed flat heads are presented in the table below. Two head types are planned for the main vessel, one CF type for low pressures at 350 MOP that has instrumentation ports, and one C-Ring type for high pressure (850 MOP) for vessel pressure testing and to be modified for a future head design (and subsequently proof tested along with a Safety Note Addendum). Stress concentration factors for the circular holes in a plate with internal pressure were used from empirical data in Wiley². Although not a perfectly matching model to Wiley, the concentration factors used are conservative. The stress concentration factor (2.278) reduced the allowable stress to 7,331 psi from 16,700 psi. Hole reinforcement requirements were also calculated using the ASME Codes. These results confirmed the thickness requirements using Wiley stress concentration factors.

Results of two types of Conflat feedthrough heads mounted to the 10.5 inch CF flange are also presented below. All head thickness calculations use the ASME head equation involving bending with the exception of the 2 3/4 inch CF where both bending and no bending cases were used. This flange was bored out to leave a head depth of 0.125" by 1.5" in diameter. The flange thickness around its mounting holes and under its knife edge remains at the nominal flange thickness of 0.5 inches. Thus, calculations were made for both and summarized below. A minimum thickness for the 1/2 inch VCR plug is calculated. The pressure side of a VCR plug is bored out 1/4 inch in diameter to this minimum thickness to be used as a gamma port.

Flange type	MOP	Required head thickness (in)	Actual head thickness (in)	Required hub thickness (in)	Actual hub thickness (in)
Conflat flange, Cu seal AAA99-104240	350	1.261	1.5	0.624	1.250
C-Ring type metal seal. AAA99-104243	850	1.247	1.980	0.661	1.250
Conflat flange, 4 5/8" Ø, x 0.750" thick. Commercial product	850	0.613	0.750	0.423	0.810

					MESN99-020-OA Page 10
1 1/3" CF	350	0.100	0.300	N/A	N/A
2 3/4" CF	350	0.178 / 0.092	0.5 / 0.125	N/A	N/A
VCR plug	850	0.052	0.052	N/A	N/A

Blind holes in the unstayed flat head were analyzed on the basis of area replacement. If the actual cross-sectional area available was greater than the cross-sectional area required, reinforcement was not required. The following table summarizes the results for the 350 MOP flat head. These calculations can also apply to blind mounting holes of the same dimension for mounting and handling the head with the caveat that hole can not be placed near other openings or reinforcements.

Hole type:	Area available (in^2)	Area required (in^2)
8-32 mini conflat holes	0.195	0.051
8-32 mounting bracket holes (internal)	0.205	0.041
1/4-28 medium conflat holes	0.250	0.125

Conflat (CF) flanges are used as connecting members and instrumentation feedthroughs in this pressure vessel design. Five 1 1/3 inch on a 5.5 inch bolt circle pattern and one 2 3/4 inch centrally located CF flanges are used on the 350 MOP head. A 4 5/8 inch CF flange is used on the detector port (850 MOP).

CF flanges were pressure tested in 1992 under the safety note END 92-072. The 1 1/3 inch nominally sized CF flanges with stainless steel bolts started leaking at \sim 15,000 psi. The 4 5/8 inch CF flange had no leakage with water as the pressure medium up to 1200 psi and minor (10⁻⁶ Torr-L/s) leaking with helium from 500 psi to 930 psi. All tests were done <u>without</u> catastrophic failure. Leakage occurred around the copper seal. A blank 2 3/4 inch was not proof tested.

For operation, the mating 1 1/3 inch CF flange to the CF port on the 350 MOP head has a high voltage feedthrough that is not rated by the manufacturer (Ceramaseal) because it is a special order. The manufacturer welded the high voltage feedthrough to an opening in the flange. LLNL has proof tested this component to burst (5850 psi). There is a concern for brittle fracture or weld failure due to cracking by mishandling that is addressed in the Fragment Hazard Mitigation paragraph below. The mating 2 3/4 inch CF flange will be proof tested at 604 psig along with the rest of the head. The mating 4 5/8 inch CF flange will be blanked off for pressure testing and initial operational tests. An addendum to this note will follow at a later date to address the attachment method of the detector to the mating flange. It will then be proof tested at 1467 psig.

Fracture Critical Components

This vessel is considered a Category IV risk according to MEDSS. Its failure has the potential for moderate injury and material testing is recommended.

The material used in this vessel is standard ASTM 304L and 316L stainless steel. Material testing was not done for the following reasons:

- (1) SA316L and SA304L are standard materials with strict manufacturing requirements.
- (2) ASME Boiler and Pressure Vessel Code does not require testing for austenitic stainless steels.
- (3) the large critical crack depths (a_{cr}) and lengths calculated using conservative stress intensity factors (K_{Ic}) from literature.
- (4) the number of cycles to failure were > 10^5 ; far larger than the $\le 10^2$ cycles expected using crack growth rates⁷ from literature.
- (5) The leak-before-break criterion is satisfied by a factor of ~10 or greater (136740 / 13824). Also, the CF type flanges used in the TPC design practically guarantee a leak before failure as demonstrated by earlier proof testing.
- (6) 316 and 304 stainless steel both have excellent toughness properties at cryogenic temperatures. Sharpy V-notch impact test data^{6,8} on 304 stainless steel indicates a slightly lowered toughness from room temperature to -196°C (150 to 124 ft-lb). For 316, the toughness lowered 13% from 141 to 122 ft-lb.

The table below summarizes the fracture toughness calculations in Appendix C.

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K _{le} (psi	K _I (psi	a _{cr}	a _{cr}	2c length of	2c length o
$\frac{1}{10} \frac{1}{2}$	$i_{n} \wedge 1/2$	True food flow	anh ante	for the second second	

	K_{lc} (psi in^1/2)	K ₁ (psi in^1/2)	a _{cr} surface flaw (in)	a _{cr} sub-surface flaw (in)	2c length of surface flaw (in)	2c length of sub-surface flaw (in)
Main vessel	136740	10115	77.3	93.6	309.3	374.2
Ellipsoidal head	136740	13824	42.2	51.1	168.9	204.4
Flat head	136740	6528	183.1	221.6	732.5	886.3

The Unbrako bolts recommended abové in the Head / Flange Calculations section are rated at their maximum tensile strength at -400° F. The alternative, 304 stainless steel fasteners have the same safe fracture critical properties as the vessel. No fracture critical calculations were performed for fasteners.

A proof test at 1.5xMAWP and at the working cryogenic temperature is planned for this vessel. Proof testing is the crux of pressure vessel qualification and is best stated from literature⁵ as follows:

"The critical flaw size associated with proof test conditions can also be used for life expectance considerations. Specifically, if a pressure vessel survives a given proof test it can be concluded that the largest defect present in the structure is

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Contents

A.	Description	3
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D.	Calculations	5
	Vessel	6
	Head / Flange Calculations	7
	Fracture Critical Components	11
	Fragment Hazard Mitigation	12
E.	Testing Requirements	13
F.	Labeling Requirements	13
G.	Associated Procedures	15
H.	References and Notes	15
APPEN	DIX A: PROOF TESTING PROCEDURE FOR THE TPC	
APPEN	IDIX B DRAWINGS	20
APPEN	IDIX C CALCULATIONS	

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A. Description

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Figure 1 – Diagram of the Time Projection Chambers (TPC)

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Associated hazards are those typical of any high pressure gas system. Failure of a vessel or component could result in either shrapnel or a blast overpressure to the body. Since the gases involved are not air, there is also the potential concern of asphyxiation. Other hazards include physical exposure to the radioactive sealed source and cold temperatures. The hazards other than those associated with the pressure vessel will be addressed by the FSP (if applicable) or separate OSP for this experiment.

C. Procedures

Design safety factors are robust for all intended pressures. The system is adequately protected by a pressure relief device at a VCR port so that components cannot be over-pressurized. This document also specifies shielding requirements for personnel protection from shrapnel in the event of an accident. However, an OSP for this experiment will address associated interlocks and operational steps required during pressurization.

D. Calculations

The following will certify the TPC for this system:

[1] <u>Hardware and Fabrication</u>

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The vessel has been designed to meet ASME Boiler and Pressure Vessel Code design guidelines. Stresses are low enough to eliminate the need for impact testing of the material in the heat effected zones created by the butt welds, UHA-51 (g) (see misc.nb calculations in Appendix C). The ASME Code also exempt austenitic, chromium-nickel stainless steels from impact testing, UHA-51(d)(1)(a). Thus, the base materials 304L and 316L are exempt.

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Most calculations were done using ASME Pressure Vessel Code, Section VIII, Division 1 guidelines. The TPC has a MAWP of 978 psig when using the C-Ring type head (no openings) and 402 psig for the Conflat type head(s) (with and without openings). A future addendum to this safety note will cover a head (with openings) to be used at 978 psig MAWP. The allowable stresses used in all calculations are based on values found in the ASME Pressure Vessel Code, Section II. For both 316L and 304L the allowable stress is 16,700 psi which provides a nominal Safety Factor of ~5 in all Pressure Vessel Code calculations (i.e., head thickness, maximum vessel pressure, minimum wall thickness, etc). The following tables are summaries of the detailed calculations found in Appendix A.

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	S1 (psi)	S2 (psi)	S3 (psi)	Von Mises (psi)	Required wall thickness (in)	Actual wall thickness (in)	If \geq 1.0 stress less than yield for 1.5xMA WP
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						MES	N99-020-OA Page 7
VCR pipe 0.5" OD	1739	4455	-978	4705	0.012	0.050	5.2
LN2 pipe 1.9" OD	1618	4214	-978	4496	0.066	0.200	5.5

Analytical results for welds, area reinforcement, and their related loads that attach the detector pipe, LN_2 pipe, and VCR pipe to the main vessel shell are detailed in the table below at a MAWP of 978 psig. Generally, if the nozzle and fillet weld load paths are greater than the total weld load, then the strengths are sufficient. The total weld load (W~(Area required – Area available)*Allowable stress)) for the VCR pipe is less than 0 because the vessel wall is 0.160" thicker than required creating much more area available than required. Thus, the area available is greater than the area removed and a negative number results.

	Area of mat'l. required (in^2)	Area of mat'l. avail. (in^2)	Total weld load (lb)	Nozzle wall load path (lb)	Fillet weld load path (lb)
Detector pipe	0.780	0.800	8172	13172	12749
LN ₂ pipe	0.504	0.508	5396	6243	6106
VCR pipe	0.134	0.194	< 0	413	402

The butt welds connecting the hub to the main vessel and the ellipsiodal head to the main vessel, the ellipsiodal head on liquid nitrogen pipe, and the hub to the detector pipe, reduced the allowable working pressure in the vessel they are connected to by 'E' (butt weld efficiency). An 'E' of 0.7 was used for these welds which reduced their associated allowable working pressures to 1421 psig, 6979 psig, and 6139 psig for the of the main vessel, LN pipe, and detector pipe respectively. Again, all of these calculated pressures use an allowable stress of 16,700 psi which has a nominal SF = 5.0 so an additional SF of 1.5 (1421 / 978) is obtained. Using a butt weld efficiency of 0.7 allows no radiography to be performed on the welds according to the ASME Boiler and Pressure Codes.

The VCR, LN_2 , and detector port openings in the vessel shell are mounted 90° to each other. The radial distance between hole centers is approximately 6.0 inches. ASME Boiler Code requires that all openings be less than the sum of their respective diameters. The maximum sum of the diameters is 3.37 inches between LN_2 and the detector port.

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Holes that do not penetrate the vessel shell may be required to horizontally mount the vessel. The depth of tapped 1/4-20 holes and 3/8-16 holes shall be ≤ 0.25 inches. Holes can not be placed near other openings or reinforcements.

Head / Flange Calculations

The following table summarizes the analytical results for the integral flange butt welded to the main access port and the small flange butt welded on the side of the

Flange	МОР	Longitudi nal hub stress (psi)	Radial flange stress (psi)	Tangential flange stress (psi)
Main 10.5" OD	850	16973	6327	4173
Main 10.5" OD	350	6388	2381	1571
Detector 4.625" OD	850	13998	2794	7367

vessel (detector port). Again, the allowable stress in 16,700 psi for the base material. Also, the ASME allowable hub stress is 1.5 time the allowable stress.

The head for operating at 850 psig, uses a C-Ring type metal seal and is made from 304L stainless steel. The (24) required bolts for this flange are Unbrako KS 1216 1/2"-13 SHCS with a tensile strength of 160,000 psi (or 304 Stainless Steel with a 81 ksi tensile strength). The main flange for operating at 350 psig is a Conflat (CF) type (304L), sealed with a soft copper flat gasket to a knife edge. The (24) required bolts for this flange are Unbrako KS 1216 1/2"-13 SHCS with a tensile strength of 160,000 psi (or 304 Stainless Steel with a 81 ksi tensile strength). All other CF flanges (1 1/3 and 2 3/4 inch) shall be bolted to the 350 MOP head using Unbrako KS 1216 psi (or 304 Stainless Steel with a 81 ksi tensile strength), 8-32 or 1/4-28 SHCS as required.

The smaller 4 5/8" CF type flange for the detector port requires 10 bolts, Unbrako KS 1216 5/16"-24 SHCS with a tensile strength of 160,000 psi (or 304 Stainless Steel with a 81 ksi tensile strength) and is made from 304L stainless steel. The following table summarizes the fastener calculations.

Flange	MOP	No. of bolts	Bolt	Torqu e (in- lb)	Flange design bolt load, operating. (lb)	Flange design bolt load, gasket seal. (lb)	Max. allowable bolt load (SF 4 applied)
Main, C-ring 10.5" OD	850	24	1/2-13	1140	58850	96913	134976
Main, CF 10.5" OD	350	24	1/2-13	1140	24677	79827	134976
Detector 4.625" OD	850	10	5/16- 24	347	10144	15452	20760
1 1/3" CF	350	6	#8-32	51	231	230	2936
2 3/4" CF	350	6	1/4-28	152	1015	527	7937

Analytical results for the commercially purchased SA316 ellipsiodal head on main vessel, nominal wall thickness 0.5 inches and the SA316 ellipsiodal head on liquid nitrogen pipe, nominal wall thickness 0.2 inches follows. The head

	MOP	Max. pressure (psig)	Required head thickness (in)	Actual head thickness (in)	If ≥ 1.0 stress less than yield for 1.5x MAWP
Main vessel	850	1513	0.320	0.500	1.03
LN ₂ pipe	850	3036	0.063	0.200	2.07

thickness calculations were done at the MAWP of 978 psig and allow for strength reduction due to the butt weld connecting them to the vessel.

Results of the unstayed flat heads are presented in the table below. Two head types are planned for the main vessel, one CF type for low pressures at 350 MOP that has instrumentation ports, and one C-Ring type for high pressure (850 MOP) for vessel pressure testing and to be modified for a future head design (and subsequently proof tested along with a Safety Note Addendum). Stress concentration factors for the circular holes in a plate with internal pressure were used from empirical data in Wiley². Although not a perfectly matching model to Wiley, the concentration factors used are conservative. The stress concentration factor (2.278) reduced the allowable stress to 7,331 psi from 16,700 psi. Hole reinforcement requirements were also calculated using the ASME Codes. These results confirmed the thickness requirements using Wiley stress concentration factors.

Results of two types of Conflat feedthrough heads mounted to the 10.5 inch CF flange are also presented below. All head thickness calculations use the ASME head equation involving bending with the exception of the 2 3/4 inch CF where both bending and no bending cases were used. This flange was bored out to leave a head depth of 0.125" by 1.5" in diameter. The flange thickness around its mounting holes and under its knife edge remains at the nominal flange thickness of 0.5 inches. Thus, calculations were made for both and summarized below. A minimum thickness for the 1/2 inch VCR plug is calculated. The pressure side of a VCR plug is bored out 1/4 inch in diameter to this minimum thickness to be used as a gamma port.

Flange type	MOP	Required head thickness (in)	Actual head thickness (in)	Required hub thickness (in)	Actual hub thickness (in)
Conflat flange, Cu seal AAA99-104240	350	1.261	1.5	0.624	1.250
C-Ring type metal seal. AAA99-104243	850	1.247	1.980	0.661	1.250
Conflat flange, 4 5/8" Ø, x 0.750" thick. Commercial product	850	0.613	0.750	0.423	0.810

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					MESN99-020-OA Page 10	
1 1/3" CF	350	0.100	0.300	N/A	N/A	
2 3/4" CF	350	0.178 / 0.092	0.5 / 0.125	N/A	N/A	
VCR plug	850	0.052	0.052	N/A	N/A	

Blind holes in the unstayed flat head were analyzed on the basis of area replacement. If the actual cross-sectional area available was greater than the cross-sectional area required, reinforcement was not required. The following table summarizes the results for the 350 MOP flat head. These calculations can also apply to blind mounting holes of the same dimension for mounting and handling the head with the caveat that hole can not be placed near other openings or reinforcements.

Hole type:	Area available (in^2)	Area required (in ²)
8-32 mini conflat holes	0.195	0.051
8-32 mounting bracket holes (internal)	0.205	0.041
1/4-28 medium conflat holes	0.250	0.125

Conflat (CF) flanges are used as connecting members and instrumentation feedthroughs in this pressure vessel design. Five 1 1/3 inch on a 5.5 inch bolt circle pattern and one 2 3/4 inch centrally located CF flanges are used on the 350 MOP head. A 4 5/8 inch CF flange is used on the detector port (850 MOP).

CF flanges were pressure tested in 1992 under the safety note END 92-072. The 1 1/3 inch nominally sized CF flanges with stainless steel bolts started leaking at \sim 15,000 psi. The 4 5/8 inch CF flange had no leakage with water as the pressure medium up to 1200 psi and minor (10⁻⁶ Torr-L/s) leaking with helium from 500 psi to 930 psi. All tests were done <u>without</u> catastrophic failure. Leakage occurred around the copper seal. A blank 2 3/4 inch was not proof tested.

For operation, the mating 1 1/3 inch CF flange to the CF port on the 350 MOP head has a high voltage feedthrough that is not rated by the manufacturer (Ceramaseal) because it is a special order. The manufacturer welded the high voltage feedthrough to an opening in the flange. LLNL has proof tested this component to burst (5850 psi). There is a concern for brittle fracture or weld failure due to cracking by mishandling that is addressed in the Fragment Hazard Mitigation paragraph below. The mating 2 3/4 inch CF flange will be proof tested at 604 psig along with the rest of the head. The mating 4 5/8 inch CF flange will be blanked off for pressure testing and initial operational tests. An addendum to this note will follow at a later date to address the attachment method of the detector to the mating flange. It will then be proof tested at 1467 psig.

Fracture Critical Components

This vessel is considered a Category IV risk according to MEDSS. Its failure has the potential for moderate injury and material testing is recommended.

The material used in this vessel is standard ASTM 304L and 316L stainless steel. Material testing was not done for the following reasons:

- (1) SA316L and SA304L are standard materials with strict manufacturing requirements.
- (2) ASME Boiler and Pressure Vessel Code does not require testing for austenitic stainless steels.
- (3) the large critical crack depths (a_{cr}) and lengths calculated using conservative stress intensity factors (K_{lc}) from literature.
- (4) the number of cycles to failure were > 10^5 ; far larger than the $\le 10^2$ cycles expected using crack growth rates⁷ from literature.
- (5) The leak-before-break criterion is satisfied by a factor of ~10 or greater (136740 / 13824). Also, the CF type flanges used in the TPC design practically guarantee a leak before failure as demonstrated by earlier proof testing.
- (6) 316 and 304 stainless steel both have excellent toughness properties at cryogenic temperatures. Sharpy V-notch impact test data^{6,8} on 304 stainless steel indicates a slightly lowered toughness from room temperature to -196°C (150 to 124 ft-lb). For 316, the toughness lowered 13% from 141 to 122 ft-lb.

The table below summarizes the fracture toughness calculations in Appendix	С.	
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	K _{Ic} (psi in^1/2)	K _l (psi in^1/2)	a _{cr} surface flaw (in)	a _{cr} sub-surface flaw (in)	2c length of surface flaw (in)	2c length of sub-surface flaw (in)
Main vessel	136740	10115	77.3	93.6	309.3	374.2
Ellipsoidal head	136740	13824	42.2	51.1	168.9	204.4
Flat head	136740	6528	183.1	221.6	732.5	886.3

The Unbrako bolts recommended abové in the Head / Flange Calculations section are rated at their maximum tensile strength at -400° F. The alternative, 304 stainless steel fasteners have the same safe fracture critical properties as the vessel. No fracture critical calculations were performed for fasteners.

A proof test at 1.5xMAWP and at the working cryogenic temperature is planned for this vessel. Proof testing is the crux of pressure vessel qualification and is best stated from literature⁵ as follows:

"The critical flaw size associated with proof test conditions can also be used for life expectance considerations. Specifically, if a pressure vessel survives a given proof test it can be concluded that the largest defect present in the structure is

smaller than the critical flaw size at the proof test conditions. Therefore, in the absence of non-destructive inspection, this flaw size can be considered the existing flaw size at the beginning of life at the operating conditions and would, in turn, serve as the basis for further crack growth consideration".

A physical inspection of the TPC for cracks is required between every experiment or experimental cycle. Careful handling of the head, vessel and its related hardware is important so that the welds attaching the various components (high voltage feedthroughs, VCR stubs) are not damaged. If any of these components are bent by mishandling, the suspect welds must be radiographicly inspected and re-proof tested.

Fragment Hazard Mitigation

A fragment deflector/stop was designed to deflect and capture a potential Ceramaseal feedthrough mishap if it were propelled from head of the vessel. It will be placed as close as practical to the TPC head and still allow operation of the vessel. The basic design is based on ballistic gun range technology where the fragment is deflected from a 45° wall into a sand trap (red arrow shows path in Figure below). All walls are made from 2.5" thick lexan that can stop the projectile if it were propelled normal into it. The opening in the stop (11" x 14") is sufficiently oversized to the Ceramaseal bolt circle diameter (5.5") and the sand trap baffle is made from 1/4" lexan to allow fragment passage. This stop will be interlocked during vessel operation. Calculation filename "fragmant.nb" in Appendix C details the shielding calculations obtained from MEDSS.



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A Kevlar drape will also be employed to shield the operator from a potential stray fragment reflected back out of the catch.

Component	Maximum Operating Pressure (psig)	Maximum Allowable Working Pressure (MAWP) (psig)	Pressure Relief Setting (psig)	Proof Test Pressure (psig)
Main Pressure Vessel	850	978	978	1467
(sketch)				
AAA99-104242 (weld				
flange)				
Flat Head, Metal C-Ring:	850	978	978	1467
AAA99-104243				
Conlfat flange, 4 5/8" Ø, x	850	978	978	1467
0.750" thick. commercial				
CF flange (blank)				
VCR Plug, 1/2"Ø,	850	978	978	1467
modified commercial				
Flat Head Conflat Type:	350	402	402	604
AAA99-104240	0.50			
Conlfat flange, 2 $3/4$ "Ø, x	350	402	402	604
0.500" thick. modified				
commercial CF flange	250	400	400	
Ceramaseal: 19543-04-CF;	350	402	402	604
1 1/3" Ø, x 0.300" thick.				
modified commercial CF				
flange	1			

The system pressure requirements are summarized as follows:

E. Testing Requirements

Detailed testing procedures have been developed and are enclosed as Appendices B. The proof test criterion for each system is 150% of MAWP.

F. Labeling Requirements

Upon completion of the testing procedures, the LLNL pressure inspector will certify the inspection of this system by completion of an LLNL Pressure Test/Inspection Record, Form LL3586, and by attaching an LLNL Pressure Tested Label, properly filled out to the individual components identified below. Appropriate additional information will be inserted as required.

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LLNL	PRES	SURE T	TESTE A	D
ASSY.	Press	ure ve	sel	
SAFETY NOT	ie Mes	SN99-	020-	0A
.M.A.W.P	978		net i l'interi Nationalité	sig,
FLUID He	, Xe, A	, CH4,	C02,	P10
TEMP. ES	20	TO a	mbier	¶ °F
REMARKS	Main Press			
TEST NO.			T.R.	
EXPIRATION	DATE			
EV		DATE	Source (



	LNL PRES	SURE TE	STED
ASSY.	AAA99	-104241-	-00
SAFETY	NOTE ME	SN99-0	20-0A
.M.A.W.P	402		PSIG.
FLUID	He, Xe, A	r, CH4, C	02, P10
TEMP.	-320	TO amb	oient °F
REMAR	4S 350 MC	OP CF Typ	e Head
TEST NO		T.I	
EXPIRA	TION DATE	leng de tengu	
BY		DATE	

Pa	nge 14
LLNL PRESSURE TESTED	
ASSY. AAA98-104240	
SAFETY NOTE MESN99-020-07	4
.M.A.W.P 402 PSI	G.
FLUID He, Xe, Ar, CH4, CO2, P1	0
TEMP 320 TO ambient	٦°
REMARKS 350 MOP CF type head	
TEST NO. T.R.	
EXPIRATION DATE	
BY	94-93 1

G. Associated Procedures

The concerns are asphyxiation, cold temperature and radiation exposure of personnel. Responsibility for an OSP resides with the user.

H. References and Notes

1. The defining drawings are as follows:

Drawing Title	<u>LLNL</u>
Pressure Chamber Lid Blank	AAA98-1104241
Pressure Chamber Lid	AAA98-1104240
Pressure Chamber Lid Blank C Ring 850 MOP	AAA98-1104243
Pressure Chamber Weld Flange 850 MOP	AAA98-1104242
Xenon Chamber Model 8" (sketch)	N/A
Xenon Chamber Model 8" associated sketches	N/A

- 2. 1995 ASME Boiler and Pressure Vessel Code, Section VIII, Division I.
- 3. Design of Piping Systems, John Wiley & Sons, Inc. 1974.
- 4. Degraded Piping Program Phase II, Sixth Program Report, Oct. 1986 September 1987, USNRC
- 5. Fracture 1969, Chapman and Hall Ltd. IBN 412094703
- 6. Handbook of Stainless Steels, D. Peckner, I. Bernstein, McGraw-Hill, 1977
- 7. Metal Fatigure in Engineering, H. Fuchs, R. Stephens, John Wiley & Sons, Inc. 1980.
- 8. Austenetic Steels at Low Temperatures, R.P. Reed, T Horiuchi, Plenum Press, 1982.

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APPENDIX A: PROOF

TESTING PROCEDURE FOR

THE TPC

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A.1 General

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This procedure is for proof testing the TPC shown in Figure 1. Initial pressure and leak tests of the system will be conducted in Building 343 because it provides an adequate barricade for conducting the test and keeps personnel exposure to a minimum. Final leak testing of joints made up after installation and retest of the systems in the future will be conducted at the B132 facility.

A.2 Hazards

The Health and Safety Manual Supplement 32.05, Section 2 – "Standard Procedure for Pressure Testing with Gas" applies.

A.3 Pretest Procedure

Use the system indicated in Figure A1 as the test source. Support the chamber horizontally. Cool the chambers' LN2 pipe and surrounding metal with an LN2 filled dewar supplied by the experimenter to simulate the thermal stresses during actual operation. Let the metal 'soak' for 20-30 minutes before proof testing.

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A.4 Test Procedure

Refer to Figure 1 and Appendix A for component designations.

A.4.1 High Pressure (1467 psig) Helium System Pressure Test

The two TPC's will first be tested to $1.5 \times MAWP$, or $1.5 \times 978 = 1467$ psig using the following components:

Vessel (2 ea., requires 2 separate proof tests) C-Ring type lid (AAA99-104243) 4 3/4" CF blank for the detector port Modified VCR plug(s) at the VCR ports

- 1. Install the hardware described above for the 1467psig proof test.
- 2. Apply 1467psig test pressure to one of the VCR ports.
- 3. Hold test pressure at 1467psig for 15 minutes.
- 4. Vent system down to 150 psig and leak check all joints under pressure with Snoop.
- 5. Vent helium to atmospheric pressure.
- A.4.2 Moderate Pressure (604 psig) Helium System Pressure Test

A single TPC will also be tested to $1.5 \times MAWP$, or $1.5 \times 402 = 604$ psig using the following components. Two tests are required to qualify both heads.

Vessel

CF type lid (AAA99-104240, AAA99-104241)

2 3/4" CF modified blank for the x-ray port

1 1/3" CF flanges with high voltage feedthroughs

4 3/4" CF blank for the detector port

Modified VCR plug at the VCR ports

- 1. Install the hardware described above for the 604 psig proof test.
- 2. Apply 604 psig test pressure to one of the VCR ports.
- 3. Hold test pressure at 604 psig for 15 minutes.
- 4. Vent system down to 150 psig and leak check all joints under pressure with Snoop.
- 5. Vent helium to atmospheric pressure.

A.4.3 Documentation

Test records shall include an LLNL Pressure test/inspection record for the separate pieces of the vessel. The pressure inspector will send the original copies of the test reports to LLNL Pressure Safety (L-384).

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APPENDIX B

DRAWINGS

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> Detector Port Date.: 2/24/99 Drawn By: Bob Patterson Material: Pipe 2 1/2 IPS sched. 80 3 16L SS 2 ea. required












MESN99-020-OA Page 27

> PumpingTubulation Date:. 2/25/99 Drawn By: Bob Patterson Material: Pipe1 1/2 IPS sched. 80 316L SS 2 ea. required



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MESN99-020-OA Page 31



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APPENDIX C

CALCULATIONS

File name	Calculations performed
Energy_vessel.nb	energy calculations, peak and static overpressure
Vessel_stress2.nb	main vessel stress calculations, wall thickness, maximum pressure, proof test stress
Ellipsoidal_head_stress.nb	main vessel head thickness, max. pressure, proof test stress
Ellipsoidal_head_stress_LN2nb	LN2 head thickness, max. pressure, proof test stress
Flange stress_hub_978.nb	main vessel C-Ring head bolt load, moment, stresses
Flange stress_hub_small_978.nb	detector port bolt load, moment, stresses
Flange stress_hub_403.nb	main vessel CF head bolt load, moment, stresses
Xe_vessel_det.nb	detector pipe stress calculations, wall thickness, maximum pressure, proof test stress
Detector_shell.nb	detector pipe weld reinforcement, area required, area available
Weld_load_stress.nb	detector pipe weld load allowable, strength of connecting elements (welds)
Xe_vessel_VCR.nb	VCR pipe stress calculations, wall thickness, maximum pressure, proof test stress
VCR_shell.nb	VCR pipe weld reinforcement, area required, area available
Weld_load_stress_VCR.nb	VCR pipe weld load allowable, strength of connecting elements (welds)
VCR_gamma_port.nb	VCR minimum head thickness calculation
Xe_vessel_LN2.nb	LN2 pipe stress calculations, wall thickness, maximum pressure, proof test stress
LN2_shell.nb	LN2 pipe weld reinforcement, area required, area available
Weld_load_stress_LN2.nb	LN2 pipe weld load allowable, strength of connecting elements (welds)
Head_350_K_openings2.nb	main vessel CF type flat head: stress concentration factor, thickness, distance between hole centers
Head_850_no_openings2.nb Head_850_4.625_no_openings2. Bolt_load_1.33CF_350.nb Bolt_load_2.75CF_350.nb Misc.nb Fracture_critical_mat'l.nb Fragmant.nb	main vessel C-ring type flat head: head thickness, hub thickness nb detector port CF type flat head: head thickness, hub thickness 1.33 CF flange bolt load, head thickness 2.75 CF flange bolt load, head thickness main vessel: distance between openings, blind mounting hole depth, reinforcement of blind holes on CF flanges mounted on 10.5" \emptyset CF flange, impact testing K _{ie} , K ₁ , critical crack lengths, Life cycles shielding calculations

(* Energy in Xenon Pressure Vessel *)

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MAWP = 978 $P_1 = MAWP$ $P_2 = 14.7$ K = 1.66 $R_i = 3.8125$ D2 = 1.5D3 = 2.32 $V_{i} = \frac{\pi (2R_{i})^{2}}{4} (12.2 - 0.5) (* in^{3} *)$ $V_2 = \frac{\pi (D2)^2}{4} (8.058 - 0.2) (* in^3 *)$ $V_3 = \frac{\pi (D3)^2}{4} 2.17 \ (* \ in^3 \ *)$ $V_{T} = V_1 + V_2 + V_3 (* in^3 *)$ Energy = $\frac{P_1 V_T}{12 (K-1)} \left(1 - \left(\frac{P_2}{P_1} \right)^{\frac{K-1}{K}} \right) (* \text{ ft-lb } *)$ Energy_{TNT} = $\frac{\text{Energy}}{3414.1}$ (* g TNT *) Energy_{1b} = Energy_{TNT} * 0.002200 (* 1b. TNT *) 978 978 14.7 1.66 3.8125 1.5 2.32 534.263 13.8862 9.1733 557.323 55852. 16.3592 0.0359903 (* From MEDSS, 30 psi is the threshold for fatalities. 0.2

to 15 psi cause physiological damage (ear, lung, etc.) However, the detailed calculation that follow (and proof tests of Conflat heads) show this vessel will leak before catastrophic failure. *)

(* The following is an analysis of the static overpressure in the confined room *)

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$P_{gov} = 1.15 \times 10^4 \frac{Energy_{1b}}{20 \times 30 \times 10} (* psig *)$]]
0.0689813	E
(* The peak overpressure is simply 6X static *)]
$P_{pov} = 6 \times P_{gov} (* psig *)$	רנ
0.413888	E

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In[12]:=
         MAWP = 978
         \sigma_{\rm a} = 16700 (*allowable stress for 316 L SST*)
         \sigma_y = 37000
         R_i = 3.8125
         R_0 = 4.3125
         t = R_o - R_i
                  Ro
         Ratio =
                   Ri
         If [1.1 < Ratio < 1.5, medium wall]</pre>
         If [Ratio < 1.1, thin wall]
         If [Ratio > 1.5, thick wall]
Out[12]= 978
Out[13]= 16700
Out[14]= 37000
Out[15] = 3.8125
Out[16]= 4.3125
Out[17] = 0.5
Out[18] = 1.13115
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Out[19]= medium wall
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A., Y

 $In[22] := (*Longitudinal Stress, S_1*)$ $S_1 = \frac{(MAWP R_1^2)}{(R_0^2 - R_1^2)}$

(*Circumferential Stress, S2*)

$$S_2 = \frac{MAWP (R_0^2 + R_1^2)}{(R_0^2 - R_1^2)}$$

(*Radial Stress, S₃*)

 $S_3 = -MAWP$

(*Von Mises Stress*)

 $\sigma_{\rm m} = \sqrt{0.5 ((S_1 - S_2)^2 + (S_2 - S_3)^2 + (S_3 - S_1)^2)}$

- Out[22]= 3499.17
- Out[23]= 7976.34

Out[24]= -978

Out(25]= 7754.69

```
(*wall thickness, in., max. pressure, psi*)
         (*Circumferential / Longitudinal Stress: wall thickness, in., max. pressure, psi*)
         E_{f} = 0.7
         (*butt weld efficiency based on no inspection, Table UW-12*)
         (*Circumferential butt welds connecting
           ellipsoidal head and hub to cylinder are Catagory A/B, Type 1 welds*)
         p = 1.67 (* in., longitudinal pitch of tube holes *)
         d = 0.5 (* in., diamnter of tube hole*)
        E_{flig} = \frac{p - d}{p} (* UG-53, Ligaments *)
         If [E_f < E_{flig}, E_f = E_f, E_f = E_{flig}]
         t_{c} = \frac{(MAWP R_{i})}{(\sigma_{a} E_{f} - 0.6 MAWP)} \quad (*UG27 \ c \ 1*)
        P_{c} = \frac{(\sigma_{a} E_{f} t)}{(R_{1} + 0.6 t)} (*UG27 \ c \ 1*)
        SF_{uc} = \frac{P_c}{MAND} (* P<sub>c</sub> uses allowable stress so SF ~5 is also inlcluded*)
        t_{1} = \frac{(MAWP R_{i})}{(2 \sigma_{a} E_{f} + 0.4 MAWP)} (*UG27 c 2*)
         P_{1} = \frac{(2 \sigma_{a} E_{f} t)}{(R_{i} - 0.4 t)} (*UG27 c 2*)
         SF_{u1} = \frac{P_1}{MAWP} (* P<sub>1</sub> uses allowable stress so SF ~5 is also inlcluded*)
         If [P_c < P_1, "circumferential stress applies", "longitudinal stress applies"]
         If [t_c > t_1, "circumferential stress applies", "longitudinal stress applies"]
Out[15]= 0.7
Out[16]= 1.67
Out[17] = 0.5
Out[18]= 0.700599
Out[19]= 0.7
Out[20] = 0.335815
```

Out[21]= 1421.28

Out[22]= 1.45325

Out[23]= 0.156855

. . Out[189]= 3235.99 Out[190]= 13.2351

Out[191] = circumferential stress applies

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Out[192] = circumferential stress applies
```

(*Check of Von Mises stress at 1.5 × MAWP for pressure test*) MAWP = 1.5 × 978

(*Longitudinal Stress,
$$S_1$$
*)
 $S_1 = \frac{(MAWP R_i^2)}{(R_o^2 - R_i^2)}$

(*Circumferential Stress, S2*)

$$S_{2} = \frac{MAWP (R_{0}^{2} + R_{1}^{2})}{(R_{0}^{2} - R_{1}^{2})}$$

(*Radial Stress, S₃*)

 $S_3 = -MAWP$

(*Von Mises Stress*)

$$\sigma_{\rm m} = \sqrt{0.5 \left(\left({{{\bf{S}}_{1}} - {{\bf{S}}_{2}}} \right)^2 + \left({{{\bf{S}}_{2}} - {{\bf{S}}_{3}}} \right)^2 + \left({{{\bf{S}}_{3}} - {{\bf{S}}_{1}}} \right)^2} \right)}$$

vessel OK at 1.5 \times MAWP during pressure test

. . . .

```
(*Xenon Pressure Vessel Stress Calculations*)
         (*Ellipsoidal Head*)
In[704]:=
           MAWP = 978
           \sigma_{a} = 16700 (*allowable stress for 304 SST*)
           \sigma_y = 32000
           D_{i} = 7.625
           t_{w} = 0.5
           (*Circumferential butt welds connecting
              ellipsoidal head and hub to cylinder are Catagory A, Type 1 welds*)
           E_f = 0.7 (*butt weld efficiency based on no inspection, Table UW-12*)
Out[704]= 978
Out[705]= 16700
Out[706]= 32000
Out[707]= 7.625
Out[708]= 0.5
Out[709]= 0.7
In[710]:= (*Wall thickness, in., max. pressure, psi*)
           (*Circumferential Stress: wall thickness, in., max. pressure, psi*)
           t_{h} = \frac{(MAWP D_{i})}{(2 \sigma_{a} E_{f} - 0.2 MAWP)} (*UG32 (d)*)
           P_{m} = \frac{(2 \sigma_{a} E_{f} t_{w})}{(D_{i} + 0.2 t_{w})} \quad (*UG32 (d)*)
           SF_{uc} = \frac{P_m 4}{MAWP}
Out[710]= 0.321649
```

Out[711] = 1513.27

Out[712]= 6.18924

្នុំទ

In[713]:=

(*Check of stress at 1.5 \times MAWP for pressure test*) MAWP = 1.5 \times 978

Solve
$$\begin{bmatrix} MAWP == & \frac{(2 \sigma E_f t_w)}{(D_i + 0.2 t_w)}, \sigma \end{bmatrix}$$

SF_y = $\frac{\sigma_y}{\sigma}$

Out[713]= 1467.

 $Out[714] = \{ \{ \sigma \rightarrow 16189.4 \} \}$

 $Out[715] = \frac{32000}{\sigma} \qquad \frac{16.700}{16,189.4} > 10$

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```
(*Xenon Pressure Vessel Stress Calculations*)
         (*Ellipsoidal Head, LN2 Trap*)
In[716]:=
           MAWP = 978
           \sigma_a = 16700 (*allowable stress for 304 SST*)
           \sigma_{\rm y}=32000
           D_1 = 1.5
           t_{w} = 0.2
            (*Circumferential butt welds connecting
             ellipsoidal head and hub to cylinder are Catagory A, Type 1 welds*)
           E_f = 0.7 (*butt weld efficiency based on no inspection, Table UW-12*)
Out[716]= 978
Out[717]= 16700
Out[718] = 32000
Out[719] = 1.5
Out[720]= 0.2
Out[721] = 0.7
In[722]:= (*Wall thickness, in., max. pressure, psi*)
            (*Circumferential Stress: wall thickness, in., max. pressure, psi*)
           t_{h} = \frac{(MAWP D_{i})}{(2 \sigma_{a} E_{f} - 0.2 MAWP)} (*UG32 (d)*)
           P_{m} = \frac{(2 \sigma_{a} E_{f} t_{w})}{(D_{i} + 0.2 t_{w})} \quad (*UG32 (d)*)
           SF_{uc} = \frac{P_m 4}{MAWP}
```

Out[722]= 0.0632753

Out[723]= 3036.36

Out[724]= 12.4187

s., 1

In[725]:=

(*Check of stress at 1.5 \times MAWP for pressure test*) MAWP = 1.5 \times 978

,

Solve [MAWP ==
$$\frac{(2 \sigma E_f t_w)}{(D_i + 0.2 t_w)}, \sigma$$
]
SF_y = $\frac{\sigma_y}{\sigma}$

Out[725] = 1467.

 $Out[726] = \{ \{ \sigma \rightarrow 8068.5 \} \}$

161700 Z (80685 (2.07) $Out[727] = \frac{32000}{\sigma}$



(5)



(* Bolted Flange Connections with Ring Type Joint *)

(* Integral Flange Type, Appendix 2, Figure 2-4 (5) shown above *) (* 850 psia MOP, custom flange, ring type joint, metal seal *) 1

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```
In[1]:= (* Bolt Load at operating conditions *)
        G = 7.980 (* Diameter, in. at gasket load location *)
        P = 978 (* MAWP, internal design pressure *)
        m = 6.5 (* gasket factor ring joint, Table 2-4.1 *)
        Ng = 0.25 (* width of ring type gasket *)
       b_o = \frac{N_g}{8} (* \text{ Table 2-5.2 (6) } *)
        If b_o <= 0.25, b = b_o, b = .5\sqrt{b_o}
        y = 26000 (* psi, design seating stress for metal seal, Table 2-5.1 *)
        H = 0.785 G^2 P (* 1b., Total hydrostatic end force *)
        H_p = 2b \times \pi GmP (* lb., Total joint-contact surface compression load *)
        W_{m1} = H + H_p (* Minimum required bolt load, for operating *)
        W_{m2} = \pi G b y (* Minimum required bolt load, for gasket seating *)
Out[1]= 7.98
Out[2]= 978
Out[3] = 6.5
Out[4] = 0.25
Out[5]= 0.03125
Out[6]= 0.03125
Out[7] = 26000
Out[8]= 48889.4
Out[9]= 9960.59
```

Out[10]= 58849.9

Out[11]= 20369.3

s., %

(* Flange Design Bolt Load*) $A_b = 0.1406 \times 24$ (*cross sectional area of 1/2-13 screw*) SF = 4 (* MEDSS *) $S_{T} = 81000$ (*Unbrako - KS 1216 1/2-13 SHCS, 160, ksi tensile strength; T = -400 $^{\circ}$ F to 1200 $^{\circ}$ F OR ASTM-A493-95 Grade S30430; 81 ksi tensile strength *) $S_a = S_T \div SF$ $L_b = S_a \times A_b$ (* lb., Max allowable bolt load *) $A_{m1} = W_{m1} / S_a$ (* in², cross-sectional area of bolts under operating condition *) $A_{m2} = W_{m2} / S_a (* in^2, cross-sectional area of bolts for gasket seating *)$ If $[A_{m1} > A_{m2}, A_m = A_{m1}, A_m = A_{m2}]$ (* in², total required cross-sectional area of bolts *) $W_o = W_{ml}$ (* lb., Flange design bolt load, for operating *) $W_g = \frac{(A_m + A_b) S_a}{2}$ (* lb., Flange design bolt load, for gasket seating *) Out[12]= 3.3744 Out[13]= 4 *Out[14]=* 81000 Out[15] = 20250Out[16]= 68331.6 Out[17]= 2.90617 Out[18]= 1.00589 Out[19]= 2.90617 Out[20]= 58849.9

Out[21] = 63590.8

×., 5

In[22]:= (* Flange Moment *) (* Table 2-6, integral flange *) C_b = 9.58 (* in., bolt circle diameter *) g1 = 0.5 (* in., hub flange thickness *) B = 7.625 (*in., inside diameter of flange *) $test = 20 g_1$ $R = \frac{(C_b - B)}{2} - g_1$ $h_D =$ $R+0.5 g_1$ (* in., radial distance from bolt circle to the circle on which h_D acts *) $h_{G} = \frac{(C_{b} - G)}{2}$ $\mathbf{h}_{\mathrm{T}} = \frac{(\mathrm{R} + \mathrm{g}_{1} + \mathrm{h}_{\mathrm{G}})}{2}$ $H_D = 0.785 B^2 P$ (* lb., total hydrostatic force on area inside of flange *) $M_D = H_D h_D$ $H_T = H - H_D$ (* lb., difference, total hydrostatic end force less H_{D} *) $M_{T} = H_{T} h_{T}$ $H_G = W_o - H (* lb., gasket load *)$ $M_G = H_G h_G$ $M_o = M_D + M_T + M_G$ (* in-lb., total flange moment due to operating conditions *) $M_g = W_o \frac{(C_b - G)}{2}$ (* in-1b., total flange moment due to gasket seating *) If $[M_o > M_g$, "operating conditions control", "gasket seating conditions control"] If $[M_o > M_g, M_o = M_o, M_o = M_\sigma]$ Out[22]= 9.58 Out(23) = 0.5Out[24]= 7.625 Out[25] = 10. Out[26]= 0.4775 Out[27]= 0.7275 Out[28]= 0.8 Out[29]= 0.88875 Out[30]= 44636.3 Out[31]= 32472.9 Out[32]= 4253.05 Out[33]= 3779.9

 $\mathcal{L}_{n} \sim$

```
Out[120]= 9960.59
Out[121]= 7968.47
Out[122] = 44221.3
Out[123] = 47080.
Out[124]= gasket seating conditions control
Out[125]= 47080.
In[126]:= (*Flange Stress *)
              e = 1 (*hub stress correction factor*)
              t = 1.25 (* in., flange thickness *)
              h = 0.125 (* in., hub length *)
              t_{e} = 2 g_{1}
              A = 10.5 (* in., OD of flange *)
              K = A / B
              T = \frac{K^2 (1 + 8.55246 \log[10, K]) - 1}{(1.04720 + 1.9448 K^2) (K - 1)} (* \text{ factor, Fig. 2-7.1*})
              U = \frac{K^2 (1 + 8.55246 \text{Log}[10, K]) - 1}{1.36136 (K^2 - 1) (K - 1)} (* \text{ factor, Fig. 2-7.1*})
              Y = \frac{1}{K-1} \left( 0.66845 + 5.71690 \frac{K^2 \log[10, K]}{(K^2 - 1)} \right) (* \text{ factor, Fig. 2-7.1*})
              Z = \frac{K^2 + 1}{r^2 - 1}  (* factor, Fig. 2-7.1*)
              g_0 = g_1
              g_1/g_o
              h_o = \sqrt{Bg_o}
              h / h_o
              V = 0.550103 (* Fig. 2-7.3 Integral flange factor *)
              d_{f} = \frac{U}{v} h_{o} g_{o}^{2}
             \mathbf{L} = \frac{\mathbf{t}_{e} + 1}{\mathbf{T}} + \frac{\mathbf{t}^{3}}{\mathbf{d}_{e}}
              S_{\rm H} = \frac{\epsilon M_{\rm o}}{L q_1^2 B} (* psi, Longitudinal hub stress *)
              S_{R} = \frac{(1.33 t_{e} + 1) M_{o}}{L t^{2} B} (* psi, Radial flange stress *)
              (* psi, Tangental flange stress *)
              S_{\rm T} = \frac{\rm Y \, M_{\rm o}}{\rm +^2 \, B} - \rm Z \, S_{\rm R}
Out[126] = 1
Out[127]= 1.25
Out[128] = 0.125
Out[129]= 1.
Out[130]= 10.5
```

A., 4

Out[131]= 1.37705

Out[132]= 1.7642

Out[133] = 6.84641

Out[134] = 6.23025

Out[135]= 3.23148

Out[136] = 0.5

Out[137] = 1.

Out[138]= 1.95256

- Out[139] = 0.0640184
- Out[140] = 0.550103
- Out[141]= 6.07525
- Out[142]= 1.45515
- Out[143]= 16972.6
- Out[144]= 6327.39

Out[145]= 4172.77

```
In[146];=
```

```
(* Allowable Flange Stress *)
```

$$\begin{split} &S_f = 16700 \; (* \; allowable \; stress \; for \; 316 \; L \; -20 \; to \; 100 \; ^{\circ}F, \; Table \; 1 \; A, \; Section \; II \; *) \\ &If [S_R < \; 1.5 \; S_f, \; "hub \; stress \; OK", \; "hub \; stress \; too \; large"] \\ &If [S_R < \; S_f, \; "radial \; stress \; OK", \; "radial \; stress \; too \; large"] \\ &If [S_T < \; S_f, \; "tangental \; stress \; OK", \; "tangental \; stress \; too \; large"] \\ &If [\frac{S_H + S_R}{2} < \; S_f, \; "average \; stress1 \; OK", \; "average \; stress1 \; too \; large"] \\ &If [\frac{S_H + S_R}{2} < \; S_f, \; "average \; stress2 \; OK", \; "average \; stress2 \; too \; large"] \end{split}$$

Out[146] = 1.6700

Out[147] = hub stress OK

Out[148] = radial stress OK

Out[149]= tangental stress OK

Out[150] = average stress1 OK

Out[151]= average stress2 OK

. . .



(5)



(* Bolted Flange Connections
with flat metal Copper Gasket, Xe chamber Detector Port *)
(* Integral Flange Type, Appendix 2, Figure 2-4 (5) shown above *)
(* 850 psia MOP, conflat type head *)

. . . . In[249]:= (* Bolt Load at operating conditions *) G = 3.35 (* Diameter, in. at gasket load location *) P = 978 (* MAWP, internal design pressure *) m = 4.75 (* gasket factor flat Cu gasket, Table 2-4.1 *) $N_g = 0.5 (* width of Cu gasket *)$ $b_o = \frac{N_g}{32}$ (* N/4 for multiple servations Table 2-5.2 (5), assume N/32 given a single knife edge serration as used in Conflats *) If $[b_o \le 0.25, b = b_o, b = .5\sqrt{b_o}]$ y = 13000 (* psi, design seating stress for soft copper, Table 2-5.1 *) $H = 0.785 G^2 P$ (* lb., Total hydrostatic end force *) $H_p = 2 b \times \pi GmP$ (* 1b., Total joint-contact surface compression load *) Wm1 = H + Hp (* Minimum required bolt load, for operating *) $W_{m2} = \pi G by$ (* Minimum required bolt load, for gasket seating *) Out[249]= 3.35 Out[250]≃ 978 Out[251]= 4.75 Out[252] = 0.5Out[253]= 0.015625 Out[254]= 0.015625 Out[255] = 13000 Out[256]= 8615.85 Out[257]= 1527.84 Out[258] = 10143.7Out[259]= 2137.76

. . . In[12]:= (* Flange Design Bolt Load*) $A_b = 0.0519 \times 10$ (*cross sectional area of 5/16-24 screw*) SF = 4 (* MEDSS *) $S_{T} = 81000$ (*Unbrako - KS 1216 5/16-24 SHCS, 160, ksi tensile strength; T = -400 °F to 1200 °F OR ASTM-A493-95 Grade S30430; 81 ksi tensile strength *) $S_a = S_T + SF$ $L_b = S_a \times A_b$ (* lb., Max allowable bolt load *) $A_{m1} = W_{m1} / S_a$ (* in², cross-sectional area of bolts under operating condition *) $A_{m2} = W_{m2} / S_a$ (* in², cross-sectional area of bolts for gasket seating *) If $[A_{m1} > A_{m2}, A_m = A_{m1}, A_m = A_{m2}]$ (* in², total required cross-sectional area of bolts *) $W_{o} = W_{m1}$ (* lb., Flange design bolt load, for operating *) $W_g = \frac{(A_m + A_b) S_a}{2}$ (* lb., Flange design bolt load, for gasket seating *) Out[12]= 0.519 Out[13]= 4 Out[14]= 81000 Out[15] = 20250Out[16]= 10509.7 Out[17]= 0.500923 Out[18]= 0.105568 Out[19]= 0.500923 Out[20]= 10143.7 Out[21]= 10326.7

. .

In[332]:= (* Flange Moment *) (* Table 2-6, integral flange *) C_b = 4.030 (* in., bolt circle diameter *) g₁ = 0.275 (* in., hub flange thickness *) B = 2.32 (*in., inside diameter of flange *) test = 20 g1 (* Refer to Appx 2, 2-3 notations, for design options *) $R = \frac{(C_b - B)}{2} - g_1$ $h_D =$ $R + 0.5 g_1$ (* in., radial distance from bolt circle to the circle on which h_D acts *) $h_{G} = \frac{(C_{b} - G)}{2}$ $\mathbf{h}_{\mathrm{T}} = \frac{(\mathrm{R} + \mathrm{g}_{\mathrm{I}} + \mathrm{h}_{\mathrm{G}})}{2}$ $H_D = 0.785 B^2 P$ (* lb., total hydrostatic force on area inside of flange *) $M_{D} = H_{D} h_{D}$ $H_T = H - H_D$ (* lb., difference, total hydrostatic end force less H_D *) $M_T = H_T h_T$ $H_G = W_o - H (* lb., gasket load *)$ $M_G = H_G h_G$ $M_o = M_D + M_T + M_G$ (* in-lb., total flange moment due to operating conditions *) $M_{g} = W_{o} \frac{(C_{b} - G)}{2}$ (* in-lb., total flange moment due to gasket seating *) If $[M_0 > M_g$, "operating conditions control", "gasket seating conditions control"] If $[M_o > M_g, M_o = M_o, M_o = M_g]$ Out[332]= 4.03 Out[333] = 0.275Out[334] = 2.32Out[335]= 5.5 Out[336] = 0.58Out[337]= 0.7175 Out[338]= 0.34 Out[339]= 0.5975 Out[340]= 4132.23 Out[341]= 2964.87 Out[342] = 4483.62Out[343]= 2678.96

.

```
Out[185] = 1527.84
Out[186]= 519.465
Out[187]= 6163.3
Out[188]= 3448.85
Out[189] = operating conditions control
Out[190]= 6163.3
In[191]:= (*Flange Stress *)
               \epsilon = 1 (*hub stress correction factor*)
               t = 0.81 (* in., flange thickness *)
              h = 0.0 (* in., hub length *)
              t_{e} = 2 g_{1}
              A = 4.63 (* in., OD of flange *)
              K = A / B
              T = \frac{K^2 (1 + 8.55246 \text{ Log}[10, K]) - 1}{(1.04720 + 1.9448 K^2) (K - 1)} (* \text{ factor, Fig. 2-7.1*})
              U = \frac{K^2 (1 + 8.55246 \log[10, K]) - 1}{1.36136 (K^2 - 1) (K - 1)} (* \text{ factor, Fig. 2-7.1*})
              Y = \frac{1}{K-1} \left( 0.66845 + 5.71690 \frac{K^2 \log[10, K]}{(K^2 - 1)} \right) (* \text{ factor, Fig. 2-7.1*})
              Z = \frac{K^2 + 1}{K^2 - 1} (* \text{ factor, Fig. 2-7.1*})
              g_0 = g_1
              g<sub>1</sub> / g<sub>o</sub>
              h_o = \sqrt{Bg_o}
              h / h_o
              V = 0.550103 (* Fig. 2-7.3 Integral flange factor *)
              d_f = \frac{U}{V} h_o g_o^2
              \mathbf{L} = \frac{\mathbf{t}_e + \mathbf{1}}{\mathbf{T}} + \frac{\mathbf{t}^3}{\mathbf{d}_e}
              S_{\rm B} = \frac{\epsilon M_{\rm o}}{L q_1^2 B} (* psi, Longitudinal hub stress *)
              S_{R} = \frac{(1.33 t_{e} + 1) M_{o}}{Lt^{2} B} (* psi, Radial flange stress *)
               (* psi, Tangental flange stress *)
              S_{\rm T} = \frac{\rm Y \, M_o}{\rm t^2 \, B} - \rm Z \, S_R
Out[191]= 1
Out[192]= 0.81
Out[193] = 0.
Out[194]= 0.55
```

Out[195]= 4.63

. Out[196]= 1.99569

Out[197] = 1.50825

Out[198]= 3.26596

Out[199] = 2.97203

Out[200] = 1.67052

Out[201] = 0.275

Out[202] = 1.

Out[203]= 0.798749

Out[204] = 0.

Out[205] = 0.550103

Out[206] = 0.358627

Out[207]= 2.50956

Out[208]= 13997.9

Out[209]= 2793.7

Out[210]= 7367.04

In[211];=

(* Allowable Flange Stress *)

$$\begin{split} & S_{\rm f} = 16700 \; (* \; \text{allowable stress for 304 L -20 to 100 °F, Table 1A, Section II *)} \\ & \text{If} \left[S_{\rm H} < 1.5 \; S_{\rm f}, \; \text{"hub stress OK", "hub stress too large"} \right] \\ & \text{If} \left[S_{\rm R} < S_{\rm f}, \; \text{"radial stress OK", "radial stress too large"} \right] \\ & \text{If} \left[S_{\rm T} < S_{\rm f}, \; \text{"tangental stress OK", "tangental stress too large"} \right] \\ & \text{If} \left[\frac{S_{\rm H} + S_{\rm R}}{2} < S_{\rm f}, \; \text{"average stress1 OK", "average stress1 too large"} \right] \\ & \text{If} \left[\frac{S_{\rm H} + S_{\rm R}}{2} < S_{\rm f}, \; \text{"average stress2 OK", "average stress2 too large"} \right] \\ & \text{If} \left[\frac{S_{\rm H} + S_{\rm T}}{2} < S_{\rm f}, \; \text{"average stress2 OK", "average stress2 too large"} \right] \end{split}$$

Out[211] = 16700

Out[212] = hub stress OK

Out[213] = radial stress OK

Out[214] = tangental stress OK

Out[215]= average stress1 OK

Out[216] = average stress2 OK







(* Bolted Flange Connections with flat metal Copper Gasket *)
(* Integral Flange Type, Appendix 2, Figure 2-4 (5) shown above *)
(* 350 psia MOP, conflat type head *)

. . .

In[184]:= (* Bolt Load at operating conditions *) G = 8.54 (* Diameter, in. at gasket load location *) P = 403 (* MAWP, internal design pressure *) m = 4.75 (* gasket factor flat Cu gasket, Table 2-4.1 *) $N_g = 0.5 (* \text{ width of Cu gasket }*)$ $b_o = \frac{N_g}{32}$ (* N/4 for multiple servations Table 2-5.2 (5), assume N/32 given a single knife edge serration as used in Conflats *) $\mathbf{b} = \mathbf{b}_{\mathbf{n}}$ y = 13000 (* psi, design seating stress for soft copper, Table 2-5.1 *) H = 0.785 G² P (* lb., Total hydrostatic end force *) $H_p = 2b \times \pi GmP$ (* 1b., Total joint-contact surface compression load *) $W_{m1} = H + H_p$ (* Minimum required bolt load, for operating *) $W_{m2} = \pi G by$ (* Minimum required bolt load, for gasket seating *) Out[184]= 8.54 Out[185] = 403Out[186]= 4.75 Out[187] = 0.5Out[188] = 0.015625Out[189]= 0.015625 Out[190] = 13000Out[191] = 23072.3Out[192]= 1604.93 Out[193]= 24677.2 Out[194]= 5449.68

In[33]:= (* Flange Design Bolt Load*) $A_b = 0.1406 \times 24$ (*cross sectional area of 1/2-13 screw*) SF = 4 (* MEDSS *) $S_{\rm T} = 81000$ (*Unbrako - KS 1216 1/2-13 SHCS, 160, ksi tensile strength; T = -400 °F to 1200 °F OR ASTM-A493-95 Grade S30430; 81 ksi tensile strength *) $S_a = S_T \div SF$ $L_b = S_a \times A_b$ (* 1b., Max allowable bolt load *) $A_{m1} = W_{m1} / S_a$ (* in², cross-sectional area of bolts under operating condition *) $A_{m2} = W_{m2} / S_a$ (* in², cross-sectional area of bolts for gasket seating *) $\texttt{If} \left[\texttt{A}_{\texttt{m1}} > \texttt{A}_{\texttt{m2}} \text{, } \texttt{A}_{\texttt{m}} = \texttt{A}_{\texttt{m1}} \text{, } \texttt{A}_{\texttt{m}} = \texttt{A}_{\texttt{m2}} \right]$ (* in², total required cross-sectional area of bolts *) $W_o = W_{m1}$ (* 1b., Flange design bolt load, for operating *) $W_g = \frac{(A_m + A_b) S_a}{2}$ (* lb., Flange design bolt load, for gasket seating *) Out[33]= 3.3744 Out[34] = 4Out[35]= 81000 Out[36]= 20250 Out[37]= 68331.6 Out[38]= 1.21863 Out[39]= 0.26912 Out[40]= 1.21863 Out[41]= 24677.2 Out[42]= 46504.4

. . .

In[205]:= (* Flange Moment *) (* Table 2-6, integral flange *) C_b = 9.58 (* in., bolt circle diameter *) g1 = 0.5 (* in., hub flange thickness *) B = 7.625 (*in., inside diameter of flange *) $test = 20 g_1$ $R = \frac{(C_b - B)}{2} - g_1$ $h_D =$ $R + 0.5 g_1$ (* in., radial distance from bolt circle to the circle on which h_D acts *) $h_{G} = \frac{(C_{b} - G)}{2}$ $\mathbf{h}_{\mathrm{T}} = \frac{(\mathrm{R} + \mathrm{g}_{1} + \mathrm{h}_{\mathrm{G}})}{2}$ $H_D = 0.785 B^2 P$ (* 1b., total hydrostatic force on area inside of flange *) $M_{D} = H_{D} h_{D}$ $H_T = H - H_D$ (* lb., difference, total hydrostatic end force less H_p *) $M_T = H_T h_T$ $H_G = W_o - H (* lb., gasket load *)$ $M_G = H_G h_G$ $M_o = M_D + M_T + M_G$ (* in-lb., total flange moment due to operating conditions *) $M_g = W_o \frac{(C_b - G)}{2}$ (* in-lb., total flange moment due to gasket seating *) If $[M_o > M_g$, "operating conditions control", "gasket seating conditions control"] $If[M_o > M_g, M_o = M_o, M_o = M_g]$ Out[205]= 9.58 Out[206]= 0.5 Out[207]= 7.625 Out[208]= 10. Out[209]= 0.4775 Out[210]= 0.7275 Out[211] = 0.52Out[212]= 0.74875 Out[213]= 18393.1 Out[214]= 13381. Out[215] = 4679.2Out[216]= 3503.55

. . .
Out[259]= 1.

Out[260]= 10.5

```
Out[250]= 1604.93
Out[251]= 834.564
Out[252]= 17719.1
Out[253]≃ 12832.1
Out[254] = operating conditions control
Out[255] = 17719.1
In[256]:= (*Flange Stress *)
              \epsilon = 1 (*hub stress correction factor*)
              t = 1.25 (* in., flange thickness *)
              h = 0.125 (* in., hub length *)
              t_{e} = 2 g_{1}
              A = 10.5 (* in., OD of flange *)
              K = A / B
              T = \frac{K^2 (1 + 8.55246 \text{Log}[10, K]) - 1}{(1.04720 + 1.9448 K^2) (K - 1)} (* \text{ factor, Fig. 2-7.1*})
              U = \frac{K^2 (1 + 8.55246 \log[10, K]) - 1}{1.36136 (K^2 - 1) (K - 1)} (* \text{ factor, Fig. 2-7.1*})
             Y = \frac{1}{K-1} \left( 0.66845 + 5.71690 \frac{K^2 \log[10, K]}{(K^2 - 1)} \right) (* \text{ factor, Fig. 2-7.1*})
              Z = \frac{K^2 + 1}{K^2 - 1}  (* factor, Fig. 2-7.1*)
              g_0 = g_1
              g<sub>1</sub> / g<sub>o</sub>
              h_o = \sqrt{Bg_o}
              h / h_o
             V = 0.550103 (* Fig. 2-7.3 Integral flange factor *)
             d_f = \frac{U}{v} h_o g_o^2
             L = \frac{t_e + 1}{T} + \frac{t^3}{d_e}
             S_{\rm H} = \frac{\epsilon M_{\rm o}}{L q_{\star}^2 B} (* psi, Longitudinal hub stress *)
             S_{R} = \frac{(1.33 t_{e} + 1) M_{o}}{L t^{2} B} (* psi, Radial flange stress *)
              (* psi, Tangental flange stress *)
             S_{T} = \frac{Y M_{o}}{+^{2} B} - Z S_{R}
Out[256]= 1
Out[257]= 1.25
Out[258]= 0.125
```

. . .

Out[261]= 1.37705

Out[262]= 1.7642

Out[263]= 6.84641

Out[264]= 6.23025

Out[265]= 3.23148

Out[266] = 0.5

Out[267] = 1.

Out[268] = 1.95256

Out[269]= 0.0640184

Out[270]= 0.550103

Out[271]= 6.07525

Out[272]= 1.45515

Out[273]= 6387.84

Out[274]= 2381.39

Out[275]= 1570.47

```
In[276]:=
```

(* Allowable Flange Stress *)

$$\begin{split} &S_f = 16700 \; (* \; allowable \; stress \; for \; 316 \; L \; -20 \; to \; 100 \; ^\circ F, \; Table \; l\,A, \; Section \; II \; *) \\ &If[S_H < 1.5 \; S_f, \; "hub \; stress \; OK", \; "hub \; stress \; too \; large"] \\ &If[S_R < S_f, \; "radial \; stress \; OK", \; "radial \; stress \; too \; large"] \\ &If[S_T < S_f, \; "tangental \; stress \; OK", \; "tangental \; stress \; too \; large"] \\ &If[\frac{S_H + S_R}{2} < S_f, \; "average \; stress1 \; OK", \; "average \; stress1 \; too \; large"] \\ &If[\frac{S_H + S_R}{2} < S_f, \; "average \; stress2 \; OK", \; "average \; stress2 \; too \; large"] \end{split}$$

Out[276]= 16700

Out[277] = hub stress OK

Out[278] = radial stress OK

Out[279] = tangental stress OK

Out[280]= average stress1 OK

Out[281]= average stress2 OK

. . v



(*Xenon Pressure Vessel Stress Calculations - Detector Port*)

1

. . .

```
In[376]:=
           MAWP = 978
           \sigma_{\rm a} = 16700 (*allowable stress for 316 L SST*)
           \sigma_{\rm y}=37000
           R_i = 1.1615
           R_{o} = 1.4375
           t = R_o - R_i
                    Ro
           Ratio =
                    Ri
           If [1.1 < Ratio < 1.5, medium wall]</pre>
           If [Ratio < 1.1, thin wall]
           If [Ratio > 1.5, thick wall]
Out[376]≃ 978
Out[377]= 16700
Out[378] = 37000
Out[379]= 1.1615
Out[380]= 1.4375
Out[381]= 0.276
Out[382]= 1.23762
```

Out[383] = medium wall

. . . In[386]:=

(*Longitudinal Stress, S₁*) $S_{1} = \frac{(MAWP R_{i}^{2})}{(R_{o}^{2} - R_{i}^{2})}$

(*Circumferential Stress, S₂*)

$$S_{2} = \frac{MAWP (R_{o}^{2} + R_{i}^{2})}{(R_{o}^{2} - R_{i}^{2})}$$

(*Radial Stress, S3*)

 $S_3 = -MAWP$

(*Von Mises Stress*)

$$\sigma_{m} = \sqrt{0.5 ((S_{1} - S_{2})^{2} + (S_{2} - S_{3})^{2} + (S_{3} - S_{1})^{2})}$$

Out[386]= 1839.34 Out[387]= 4656.68 Out[388]= -978 Out[389]= 4879.78

.

In[42]:= (*wall thickness, in., max. pressure, psi*) (*Circumferential Stress: wall thickness, in., max. pressure, psi*) $E_f = 0.7$ (*butt weld efficiency based on no inspection, Table UW-12*) $t_{c} = \frac{(MAWP R_{i})}{(\sigma_{a} E_{f} - 0.6 MAWP)} (*UG27 c 1*)$ $P_{c} = \frac{(\sigma_{a} E_{f} t)}{(R_{i} + 0.6 t)} (*UG27 c 1*)$ $SF_{uc} = \frac{P_c}{MAMD}$ (* P_c uses allowable stress so SF ~5 is also inlcluded*) (*Longitudinal Stress: wall thickness, in., max. pressure, psi*) (*Circumferential butt welds connecting ellipsoidal head and hub to cylinder are Catagory A, Type 1 welds*) $E_f = 0.7$ (*butt weld efficiency based on no inspection, Table UW-12*) $t_1 = \frac{(MAWP R_i)}{(2 \sigma_a E_f + 0.4 MAWP)} \quad (*UG27 \ c \ 2*)$ $P_{1} = \frac{(2 \sigma_{a} E_{f} t)}{(R_{1} - 0.4 t)} (*UG27 c 2*)$ $SF_{ul} = \frac{P_1}{MaWP}$ (* P_1 uses allowable stress so SF ~5 is also inlcluded*) If $[P_c < P_1, "circumferential stress applies", "longitudinal stress applies"]$ If $[t_c > t_1, "circumferential stress applies", "longitudinal stress applies"]$ Out[42] = 0.7Out[43]= 0.102308 Out[44] = 2431.2Out[45] = 2.48589Out[46] = 0.7Out[47]= 0.0477867 Out[48]= 6139.17 Out[49]= 6.27727 Out[50]= circumferential stress applies Out[51] = circumferential stress applies

. . .

In[400]:=
 (*Check of Von Mises stress at 1.5 × MAWP for pressure test*)
 MAWP = 1.5 × 978
 (*Longitudinal Stress, S₁*)
 (MAWP P.²)

$$S_1 = \frac{(MAWP R_1^2)}{(R_0^2 - R_1^2)}$$

(*Circumferential Stress, S₂*)

$$S_{2} = \frac{MAWP (R_{o}^{2} + R_{i}^{2})}{(R_{o}^{2} - R_{i}^{2})}$$

(*Radial Stress, S₃*)

 $S_3 = -MAWP$

_

(*Von Mises Stress*)

$$\sigma_{m} = \sqrt{0.5 ((S_{1} - S_{2})^{2} + (S_{2} - S_{3})^{2} + (S_{3} - S_{1})^{2})}$$

$$N_r = \frac{\sigma_y}{\sigma_m}$$

If [N_r > 1, "vessel OK at 1.5 × MAWP during pressure test"]

Out[400]= 1467.

Out[401]= 2759.01

Out[402]= 6985.02

Out[403] = -1467.

Out[404]= 7319.66

Out[405] = 5.05488

Out[406] = vessel OK at 1.5 × MAWP during pressure test



(This Figure Illustrates a Common Nozzle Configuration and is Not Intended to Prohibit Other Configurations Permitted by the Code.)

```
(*Opening reinforcement calculations*)
         (* Detector pipe to shell wall*)
         (* A3 = 0, A5 = 0, A42 = 0 *)
         (* Sch 80 Pipe, 3 " Ø *)
        Tx = 2.875 (*OD*)
        d = 2.323 (*ID min*)
        tn = (Tx - d) / 2 (*nozzel wall thickness*)
        te = 1.25 * tn (*weld leg height*)
Out[445] = 2.875
Out[446] = 2.323
Out[447]= 0.276
Out[448] = 0.345
In[473]:= F = 1 (*correction factor*)
           tr = 0.335815 (*minimum shell thickness, Vessel_stress2.nb*)
           fr1 = 1 (*strength reducton factor*)
           t = 0.5 (*shell wall thickness*)
           E1 = 1 (*joint efficiency*)
           \mathbf{A} = \mathbf{d} \mathbf{tr} \mathbf{F} + 2 \mathbf{tn} \mathbf{tr} \mathbf{F} (1 - \mathbf{fr} \mathbf{1})
           Ala = d (Elt - Ftr) - 2tn (Elt - Ftr) (1 - fr1)
           A1b = 2 (t + tn) (E1t - Ftr) - 2tn (E1t - Ftr) (1 - fr1)
             If [A1a > A1b, A1 = A1a, A1 = A1b]
Out[473] = 1
Out[474] = 0.335815
Out[475]= 1
Out[476]= 0.5
Out[477] = 1
Out[478]= 0.780098
Out[479] = 0.381402
Out[480] = 0.254815
Out[481] = 0.381402
```

2

```
In[482]:= fr2 = 1 (*strength reducton factor*)
          trn = 0.10230807 (*requierd nozzel thickness, Xe_vessel_det.nb*)
          A2a = 5 (tn - trn) fr2t
          A2b = 5 (tn - trn) fr2 tn
          If [A2a < A2b, A2 = A2a, A2 = A2b]
Out[482]= 1
Out[483]= 0.10230807
Out[484]= 0.43423
Out[485]= 0.239695
Out[486]= 0.239695
        fr3 = 1 (*strength reducton factor*)
       A43 = te^2 fr3
       A41 = \frac{te^2 fr3}{2} (* 1/2 the area, skip weld on outside*)
Out[492]= 1
Out[493] = 0.119025
Out[494]= 0.0595125
In[498]:= (A1 + A2 + A43 + A41)
          А
          (A1 + A2 + A43 + A41) >= A
          (*If actual area > area required, then no additional reinforcement required *)
Out[498]= 0.799634
Out[499]= 0.780098
Out[500]= True
```

. . .



(*must run "detector_shell.nb" file first to save variables defined below into memory*)

```
In[523]:= (*Load / Stress Carried by Welds*)
           A
           A1
          A2
          A3 = 0
          A5 = 0
           A41
           A42 = 0
           A43
Out[523]= 0.780098
Out[524] = 0.381402
Out[525] = 0.239695
Out[526]= 0
Out[527]= 0
Out[528]= 0.0595125
Out[529]= 0
Out[530]= 0.119025
In[533]:= Sv = 16700 (* allowable stress*)
           W = (A - A1 + 2 \operatorname{tn} \operatorname{fr1} (E1t - Ftr)) Sv
Out[533] = 16700
Out[534]= 8171.75/
In[535]:=
           W_{1-1} = (A2 + A5 + A41 + A42) Sv
Out[535]= 4996.76
In[536] := W_{2-2} = (A2 + A3 + A41 + A43 + 2 tn t fr1) Sv
Out[536]= 11593.7
In[537]:=
          W_{3-3} = (A2 + A3 + A5 + A41 + A42 + A43 + 2 tn t fr1) Sv
Out[537]= 11593.7
        (* W (total weld load) << W_{1-1}, W_{2-2}, W_{3-3}, (weld load available)*)
In[539]:= (*Allowable Unit Stresses*)
           (*Fillet Weld Shear, UW 15 c*)
           \sigma_{\text{fw}} = 0.49 \text{ (Sv)}
Out[539]= 8183.
```

```
In[540]:= (*Nozzel Wall Shear, UG 45 c*)
            \sigma_{nw} = 0.7 (Sv)
Out[540] = 11690.
In[541]:=
            (*Strength of Connection Elements*)
            (*Fillet Weld Shear*)
           W_{fw} = \frac{\pi}{2} Tx te \sigma_{fw}
Out[541]= 12749.4
In[542]:=
            (*Strength of Connection Elements*)
            (*Nozzel Wall Shear*)
           W_{nw} = \frac{\pi}{2} \frac{(Tx+d)}{2} tn \sigma_{nw}
Out[542]= 13171.9
In[543]:=
            WS_{1-1} = W_{nw}
            WS_{2-2} = W_{fw}
Out[543]= 13171.9
Out[544]= 12749.4
         (*All Paths WS_{1\text{-}1},\ WS_{2\text{-}2}, are stronger than the required strength W*)
```

3

.



(*Xenon Pressure Vessel Stress Calculations - VCR Port*)

```
In[545]:=
           MAWP = 978
           \sigma_a = 16700 (*allowable stress for 316 L SST*)
           \sigma_{\rm y}=37000
          R_i = 0.40 / 2.
          R_o = 0.5 / 2.
           t = R_o - R_i
                    R_{o}
           Ratio =
                    Ri
           If [1.1 < Ratio < 1.5, medium wall]</pre>
           If [Ratio < 1.1, thin wall]
           If [Ratio > 1.5, thick wall]
Out[545]= 978
Out[546] = 16700
Out[547]= 37000
Out[548] = 0.2
Out[549]= 0.25
Out[550] = 0.05
Out[551] = 1.25
Out[552] = medium wall
```

In[555]:=

(*Longitudinal Stress, $S_1 \star$) $S_1 = \frac{(MAWP R_1^2)}{(R_0^2 - R_1^2)}$

(*Circumferential Stress, S₂*)

$$S_{2} = \frac{MAWP (R_{o}^{2} + R_{i}^{2})}{(R_{o}^{2} - R_{i}^{2})}$$

(*Radial Stress, S₃*)

 $S_3 = -MAWP$

(*Von Mises Stress*)

$$\sigma_{\rm m} = \sqrt{0.5 \left(\left({{{\rm{S}}_{\rm{1}}} - {{\rm{S}}_{\rm{2}}} \right)^2 + \left({{{\rm{S}}_{\rm{2}}} - {{\rm{S}}_{\rm{3}}} \right)^2 + \left({{{\rm{S}}_{\rm{3}}} - {{\rm{S}}_{\rm{1}}} \right)^2} \right)}$$

- Out[555]= 1738.67
- Out[556]= 4455.33
- Out[557]= -978
- Out[558]= 4705.4

In[73]:= (*wall thickness, in., max. pressure, psi*) (*Circumferential Stress: wall thickness, in., max. pressure, psi*) Ef = 1.0 (*efficiency*) $t_{c} = \frac{(MAWP R_{i})}{(\sigma_{a} E_{f} - 0.6 MAWP)} (*UG27 c 1*)$ $P_{c} = \frac{(\sigma_{a} E_{f} t)}{(R_{i} + 0.6 t)} (*UG27 c 1*)$ $SF_{uc} = \frac{P_c}{Maturb}$ (* P_c uses allowable stress so SF ~5 is also inlcluded*) (*Longitudinal Stress: wall thickness, in., max. pressure, psi*) (*Circumferential butt welds connecting ellipsoidal head and hub to cylinder are Catagory A, Type 1 welds*) Ef = 1.0 (*efficincy*) $t_{1} = \frac{(MAWP R_{i})}{(2 \sigma_{a} E_{f} + 0.4 MAWP)} (*UG27 c 2*)$ $P_{1} = \frac{(2 \sigma_{a} E_{f} t)}{(R_{i} - 0.4 t)} (*UG27 \ c \ 2*)$ $SF_{ul} = \frac{P_1}{MaWP}$ (* P₁ uses allowable stress so SF ~5 is also inlcluded*) If $[P_c < P_1, "circumferential stress applies", "longitudinal stress applies"]$ If $[t_c > t_1, "circumferential stress applies", "longitudinal stress applies"]$ Out[73] = 1.Out[74]= 0.0121391 Out[75]= 3630.43 Out[76]= 3.7121 Out[77] = 1.Out[78]= 0.00578849 Out[79]= 9277.78 Out[80]= 9.48648 Out[81] = circumferential stress applies Out[82] = circumferential stress applies

, S In[569]:=

(*Check of Von Mises stress at 1.5 \times MAWP for pressure test*) MAWP = 1.5 \times 978

(*Longitudinal Stress,
$$S_1$$
*)
 $S_1 = \frac{(MAWP R_1^2)}{(R_o^2 - R_1^2)}$

(*Circumferential Stress, S2*)

$$S_{2} = \frac{MAWP (R_{o}^{2} + R_{i}^{2})}{(R_{o}^{2} - R_{i}^{2})}$$

(*Radial Stress, S₃*)

 $S_3 = -MAWP$

(*Von Mises Stress*)

$$\sigma_{\rm m} = \sqrt{0.5 \left(\left({{{\rm{S}}_{\rm{1}}} - {{\rm{S}}_{\rm{2}}} \right)^2 \ + \ \left({{{\rm{S}}_{\rm{2}}} - {{\rm{S}}_{\rm{3}}} \right)^2 \ + \ \left({{{\rm{S}}_{\rm{3}}} - {{\rm{S}}_{\rm{1}}} \right)^2} \right)}$$

$$N_{r} = \frac{\sigma_{y}}{\sigma_{m}}$$

If [N_r > 1, "vessel OK at 1.5 × MAWP during pressure test"]

,

Out [569] = 1467.

Out[570]= 2608.

Out[571]= 6683.

Out[572] = -1467.

Out[573]= 7058.11

Out[574]= 5.2422

Out(575)= vessel OK at 1.5 × MAWP during pressure test



```
In[576]:= (* Opening Reinforcement Calculations*)
           (* VCR Gland to shell wall*)
           (* A3 = 0, A5 = 0, A43 = 0, A42 = 0 *)
           (* VCR, 0.5 " Ø *)
           Tx = .5 (*OD*)
           d = 0.40 (*ID min*)
           tn = (Tx - d) / 2 (*nozzel wall thickness*)
           te = 1.25 * tn (*weld leg height*)
Out[576]= 0.5
Out[577] = 0.4
Out[578]= 0.05
Out[579]= 0.0625
In[580]:= F = 1 (*correction factor*)
           tr = 0.335815 (*minimum shell thickness, Vessel_stress2.nb*)
           fr1 = 1 (*strength reducton factor*)
          t = 0.5 (*shell wall thickness*)
          E1 = 1 (*joint efficiency*)
          \mathbf{A} = \mathbf{d} \mathbf{tr} \mathbf{F} + \mathbf{2} \mathbf{tn} \mathbf{tr} \mathbf{F} (\mathbf{1} - \mathbf{fr} \mathbf{1})
           Ala = d(Elt - Ftr) - 2tn(Elt - Ftr)(1 - fr1)
           A1b = 2 (t + tn) (E1t - Ftr) - 2tn (E1t - Ftr) (1 - fr1)
             If [A1a > A1b, A1 = A1a, A1 = A1b]
Out[580]= 1
Out[581]= 0.335815
Out[582]= 1
Out[583]= 0.5
Out[584]= 1
Out[585] = 0.134326
Out[586]= 0.065674
Out[587]= 0.180604
Out[588]= 0.180604
```

. . .

```
In[589]:= fr2 = 1 (*strength reducton factor*)
         trn = 0.0121391(*required nozzel thickness, Xe_vessel_VCR.nb*)
         A2a = 5 (tn - trn) fr2 t
         A2b = 5 (tn - trn) fr2 tn
         If [A2a < A2b, A2 = A2a, A2 = A2b]
Out[589]= 1
Out[590]= 0.0121391
Out[591]= 0.0946522
Out[592] = 0.00946522
Out[593]= 0.00946522
In[594]:= fr3 = 1 (*strength reducton factor*)
         A43 = te^2 fr3
Out[594]= 1
Out[595]= 0.00390625
In[596]:= (A1 + A2 + A43)
         А
          (A1 + A2 + A43) >= A
          (*If actual area > area required, then no additional reinforcement required *)
Out[596]= 0.193975
Out[597]= 0.134326
Out[598]= True
```



(*must run "VCR_shell.nb" file first to save variables defined below into memory*)

. . . .

```
In[599]:= (*Load / Stress Carried by Welds*)
           A
           A1
          A2
           A3 = 0
           \mathbf{A5} = \mathbf{0}
           A41 = 0
           A42 = 0
           A43
Out[599]= 0.134326
Out[600]= 0.180604
Out[601]= 0.00946522
Out[602]= 0
Out[603]= 0
Out[604] = 0
Out[605]= 0
Out[606]= 0.00390625
In[607] := Sv = 16700
          W = (A - A1 + 2 \operatorname{tn} \operatorname{fr1} (E1t - Ftr)) Sv
Out[607]= 16700
Out[608] = -498.645
In[610]:=
           W_{1-1} = (A2 + A5 + A41 + A42) Sv
Out[610]= 158.069
In[611] := W_{2-2} = (A2 + A3 + A41 + A43 + 2 tn t fr1) Sv
Out[611] = 1058.3
In[612] := W_{3-3} = (A2 + A3 + A5 + A41 + A42 + A43 + 2 tn t fr1) Sv
Out[612]= 1058.3
        (* W (total weld load) << W_{1-1}, W_{2-2}, W_{3-3}, (weld load available)*)
In[613]:= (*Allowable Unit Stresses*)
           (*Fillet Weld Shear, UW 15 c*)
           \sigma_{fw} = 0.49 (Sv)
Out[613]= 8183.
```

. . . .

```
In[614]:= (*Nozzel Wall Shear, UG 45 c*)
            \sigma_{nw} = 0.7 (Sv)
Out[614]= 11690.
In[615]:=
            (*Strength of Connection Elements*)
            (*Fillet Weld Shear*)
            W_{fw} = \frac{\pi}{2} \operatorname{Tx} te \sigma_{fw}
Out[615]= 401.682
In[616]:≃
            (*Strength of Connection Elements*)
            (*Nozzel Wall Shear*)
            W_{nw} = \frac{\pi}{2} \frac{(Tw+d)}{2} tn \sigma_{nw}
Out[616]= 413.159
In[617]:=
            WS_{1-1} = W_{nw}
            WS_{2-2} = W_{fw}
Out[617]= 413.159
Out[618]= 401.682
```

(*All Paths $WS_{1\text{-}1},\ WS_{2\text{-}2},$ are stronger than the required strength W*)

,

```
(* VCR Port Xe chamber gamma ray feedthru *)
        (* 850 psia MOP,
         stainless steel VCR plug with 0.250 " Ø counterbore. Determine head thickness: *)
In[24]:= (* Load at operating conditions *)
         G = 0.250 (* Diameter, in. at gasket load location *)
         P = 850 * 1.15 (* MAWP, internal design pressure *)
         H = 0.785 G^2 P (* lb., Total hydrostatic end force *)
Out[24] = 0.25
Out[25]= 977.5
Out[26]= 47.9586
In[27]:=
         C_{a} = 0.75
                     (*Head attachment constant, UG-34 (r)*)
         E<sub>f</sub> = 1.0 (*Efficiency Factor *)
         d<sub>ga</sub> = G (*in. hole cross-sectional diameter*)
         \sigma_u = 77000.0 \; (*psi, 316 L \; ultimate \; strength*)
         \sigma_a = 16700 (*psi, 316 L allowable strength*)
         th = d_{ga} \sqrt{\frac{C_a \times P}{\sigma_a \times E_f}} (* in., required head thickness, no bending moment *)
Out[27] = 0.75
Out[28]= 1.
Out[29]= 0.25
Out[30]= 77000.
Out[31]= 16700
Out[32]= 0.0523806
```



(*Xenon Pressure Vessel Stress Calculations - LN2 Port*)

```
In[619]:=
          MAWP = 978
          \sigma_a = 16700 (*allowable stress for 316 L SST*)
          \sigma_{\rm y}=37000
          R_i = 1.5 / 2.
          R_o = 1.9/2.
          t = R_o - R_i
                    R_{o}
          Ratio =
                    Ri
           If [1.1 < Ratio < 1.5, medium wall]
           If [Ratio < 1.1, thin wall]
          If [Ratio > 1.5, thick wall]
Out[619]= 978
Out[620]= 16700
Out[621] = 37000
Out[622] = 0.75
Out[623] = 0.95
Out[624] = 0.2
Out[625]= 1.26667
```

Out[626] = medium wall

.

----- In[629]:=

(*Longitudinal Stress, S_1 *) $S_1 = \frac{(MAWP R_i^2)}{(R_o^2 - R_i^2)}$

(*Circumferential Stress, S₂*)

$$S_{2} = \frac{MAWP (R_{o}^{2} + R_{i}^{2})}{(R_{o}^{2} - R_{i}^{2})}$$

(*Radial Stress, S₃*)

 $S_3 = -MAWP$

(*Von Mises Stress*)

$$\sigma_{\rm m} = \sqrt{0.5 \left(\left({{{\rm{S}}_{\rm{1}}} - {{\rm{S}}_{\rm{2}}} \right)^2 + \left({{{\rm{S}}_{\rm{2}}} - {{\rm{S}}_{\rm{3}}} \right)^2 + \left({{{\rm{S}}_{\rm{3}}} - {{\rm{S}}_{\rm{1}}} \right)^2} \right)}$$

- Out[629]= 1618.01
- Out[630]= 4214.03
- Out[631]= -978
- Out[632]= 4496.43

In[104]:= (*wall thickness, in., max. pressure, psi*) (*Circumferential Stress: wall thickness, in., max. pressure, psi*) $E_f = 0.7$ (*butt weld efficiency based on no inspection, Table UW-12*) $t_{c} = \frac{(MAWP R_{i})}{(\sigma_{a} E_{f} - 0.6 MAWP)} \quad (*UG27 \ c \ 1*)$ $P_{c} = \frac{(\sigma_{a} E_{f} t)}{(R_{i} + 0.6 t)} (*UG27 c 1*)$ $SF_{uc} = \frac{P_c}{MaWD}$ (* P_c uses allowable stress so SF ~5 is also inlcluded*) (*Longitudinal Stress: wall thickness, in., max. pressure, psi*) (*Circumferential butt welds connecting ellipsoidal head and hub to cylinder are Catagory A, Type 1 welds*) $E_{f} = 0.7$ (*butt weld efficiency based on no inspection, Table UW-12*) $t_{1} = \frac{(MAWP R_{1})}{(2 \sigma_{a} E_{f} + 0.4 MAWP)} (*UG27 c 2*)$ $P_{1} = \frac{(2 \sigma_{a} E_{f} t)}{(R_{i} - 0.4 t)} (*UG27 c 2*)$ $SF_{u1} = \frac{P_1}{MaWP}$ (* P₁ uses allowable stress so SF ~5 is also inlcluded*) If $[P_c < P_1, "circumferential stress applies", "longitudinal stress applies"]$ If $[t_c > t_1, "circumferential stress applies", "longitudinal stress applies"]$ Out[104] = 0.7Out[105]= 0.066062 Out[106]= 2687.36 Out[107]= 2.74781 Out[108] = 0.7Out[109]= 0.0308567 Out[110] = 6979.1 Out[111]= 7.1361 Out[112] = circumferential stress applies Out[113] = circumferential stress applies

. . In[643]:=
 (*Check of Von Mises stress at 1.5 × MAWP for pressure test*)
 MAWP = 1.5 × 978
 (*Longitudinal Stress, S₁*)

$$S_{1} = \frac{(MAWP R_{1}^{2})}{(R_{0}^{2} - R_{1}^{2})}$$

(*Circumferential Stress, S2*)

$$S_{2} = \frac{MAWP (R_{o}^{2} + R_{i}^{2})}{(R_{o}^{2} - R_{i}^{2})}$$

(*Radial Stress, S₃*)

 $S_3 = -MAWP$

_

(*Von Mises Stress*)

$$\sigma_{\rm m} = \sqrt{0.5 \left(\left({{{\rm{S}}_{\rm{1}}} - {{\rm{S}}_{\rm{2}}} \right)^2 + \left({{{\rm{S}}_{\rm{2}}} - {{\rm{S}}_{\rm{3}}} \right)^2 + \left({{{\rm{S}}_{\rm{3}}} - {{\rm{S}}_{\rm{1}}} \right)^2} \right)}$$

$$N_{r} = \frac{\sigma_{y}}{\sigma_{m}}$$

If [N_r > 1, "vessel OK at 1.5 × MAWP during pressure test"]

,

Out[643]= 1467.

Out[644]= 2427.02

Out[645]= 6321.04

Out[646] = -1467.

Out[647]= 6744.64

Out[648] = 5.48583

Out[649]= vessel OK at 1.5 × MAWP during pressure test



```
In[4]:= (* Opening Reinforcement Calculations*)
        (* LN2 Trap to shell wall*)
        (* A3 = 0, A5 = 0, A42 = 0 *)
        (* Pipe Sch. 80 1.5 " Ø *)
        Tx = 1.9 (*OD*)
        d = 1.5 (*ID min*)
        tn = (Tx-d) / 2 (*nozzel wall thickness*)
        te = 1.25 * tn (*weld leg height*)
Out[4] = 1.9
Out[5] = 1.5
Out[6]= 0.2
Out[7] = 0.25
In[8]:= F = 1 (*correction factor*)
        tr = 0.335815 (*minimum shell thickness, Vessel_stress2.nb*)
        fr1 = 1 (*strength reducton factor*)
        t = 0.5 (*shell wall thickness*)
       E1 = 1 (*joint efficiency*)
        A = dtr F + 2tntr F (1 - fr1)
        A1a = d (E1t - Ftr) - 2tn (E1t - Ftr) (1 - fr1)
        Alb = 2 (t + tn) (Elt - Ftr) - 2 tn (Elt - Ftr) (1 - fr1)
          If [A1a > A1b, A1 = A1a, A1 = A1b]
Out[8]= 1
Out[9]= 0.335815
Out[10]= 1
Out[11] = 0.5
Out[12] = 1
Out[13] = 0.503722
Out[14] = 0.246278
Out[15]= 0.229859
Out[16]= 0.246278
```

```
In[17]:= fr2 = 1 (*strength reducton factor*)
         trn = 0.066062 (*required nozzel thickness, Xe_vessel_LN2.nb*)
         A2a = 5 (tn - trn) fr2t
         A2b = 5 (tn - trn) fr2 tn
         If [A2a < A2b, A2 = A2a, A2 = A2b]
Out (17) = 1
Out[18] = 0.066062
Out[19] = 0.334845
Out[20]= 0.133938
Out[21]= 0.133938
In[72]:= fr3 = 1 (*strength reducton factor*)
         A43 = te^2 fr3
         te_o = 1.4 tn
         A41 = \frac{te_o^2 fr3}{1.2} (* 80% the area, skip weld on outside*)
Out[72] = 1
Out[73]= 0.0625
Out[74] = 0.28
Out[75]= 0.0653333
In[76]:= (A1 + A2 + A43 + A41)
         А
         (A1 + A2 + A43 + A41) >= A
         (*If actual area > area required, then no additional reinforcement required *)
Out[76]= 0.508049
Out[77]= 0.503722
Out[78]= True
```



(*must run "LN2_shell.nb" file first to save variables defined below into memory*)

```
In[79]:= (*Load / Stress Carried by Welds*)
          А
         A1
         A2
         A3 = 0
         A5 = 0
         A41
         A42 = 0
         A43
Out[79] = 0.503722
Out[80] = 0.246278
Out[81]= 0.133938
Out[82]= 0
Out[83]= 0
Out[84]= 0.0653333
Out[85]= 0
Out[86]= 0.0625
In[87] := Sv = 16700
         W = (A - A1 + 2 \operatorname{tn} \operatorname{fr1} (E1 t - F tr)) Sv
Out[87] = 16700
Out[88]= 5396.09
In[89]:=
         W_{1-1} = (A2 + A5 + A41 + A42) Sv
Out[89]= 3327.83
In[90] := W_{2-2} = (A2 + A3 + A41 + A43 + 2 tn t fr1) Sv
Out[90]= 7711.58
        W_{3-3} = (A2 + A3 + A5 + A41 + A42 + A43 + 2 tn t fr1) Sv
        7664.26
        (* W (total weld load) << W_{1-1}, W_{2-2}, W_{3-3}, (weld load available)*)
In[91]:= (*Allowable Unit Stresses*)
          (*Fillet Weld Shear, UW 15c*)
         \sigma_{fw} = 0.49 (Sv)
```

. . .

```
In[92] := (*Nozzel Wall Shear, UG 45 c*)

\sigma_{nw} = 0.7 (Sv)
```

Out[92]= 11690.

In[93]:=

(*Strength of Connection Elements*) (*Fillet Weld Shear*)

$$W_{fw} = \frac{\pi}{2} \operatorname{Txte} \sigma_{fw}$$

Out[93] = 61.05.57

In[94]:=

(*Strength of Connection Elements*) (*Nozzel Wall Shear*)

$$W_{nw} = \frac{\pi}{2} \frac{(Tx + d)}{2} tn \sigma_{nw}$$

Out[94]= 6243.29

In[95]:=

 $WS_{1-1} = W_{nw}$ $WS_{2-2} = W_{fw}$

Out[95]= 6243.29

Out[96]= 6105.57

(*All Paths $WS_{1\text{-}1}\text{, }WS_{2\text{-}2}\text{,}$ are stronger than the required strength W*)
(* Stress Concentration Factor for mini-conflat openings in head. Reference: Wiley *)

Stress Concentration Factors

	Pattern	Spacing	Maximum K,	Location	Reference
1	r e R 30°	r/R = 0.5	See Fig. 126	See Fig. 126	223,228,229
2	A T	$R/R_0 = 0.5$ $r/R_0 = 0.2$	See Fig. 127	See Fig. 127	230
3	A CORD	$R/R_0 = 0.5$ r/R_0 = 0.2	See Fig. 127	See Fig. 127	230
		$R/R_0 = 0.5$ $r/R_0 = 0.25$	2. 45	A	223
4	B C C C R	$R/R_0 = 0.6$ $r/R_0 = 0.2$	2. 278 Pressure in All Holes 1. 521	A	223
	A 300 300		Pressure in Center Hole Only	B	

Table 4 Maximum K_t for circular plate with circular holes with internal pressure only

```
In[1039]:= (*must run "Flange stress_hub_403.nb"
             file first to save variables defined below into memory*)
           (* Assumptions: Chamber head design has 5 mini-conflat holes, not 6,
            K_t will be conservative. Chamber head has 1.5 " diameter inner hole, #4 model has
             equal diameter holes throughout, Kt will not be conservative. Assume
             these 2 opposites have a cancelling effect and given K_t is valid. Actual BC hole
             radius is 0.3125". But, for this analysis assume all holes 0.75" radius *)
           Ro = 5.25 (*in., Flange outside radius*)
           r<sub>h</sub> = 0.750 (*in., BC hole radius*)
           Ri = 0.750 (*in., inner hole radius*)
           R = 5.5/2 (* in., mini conflat bolt circle radius *)
           1 = \frac{Ri}{Ro} \; (*graph \; constant*)
           m = \frac{R}{Ro} (*graph constant*)
           o = \frac{r_h}{Ro} (*graph constant*)
Out[1039]= 5.25
Out[1040]= 0.75
Out[1041]= 0.75
Out[1042]= 2.75
Out[1043]= 0.142857
Out[1044]= 0.52381
Out[1045]= 0.142857
In[1256]:= (* \frac{R}{Ro} and \frac{r_h}{Ro} are slightly less than #4 model,
            but K_t will be less (conservative) for chamber head design. \star)
            K_{t} = 2.278
Out[1256]= 2.278
```

. .

```
In[1257]:=
             C_{e} = 0.3
                        (*flange attachment constant*)
             p = 350 \times 1.15 (*psi, MAWP*)
             E_{f} = 1.0
                        (*Efficiency Factor *)
             d<sub>ga</sub> = 8.54 (*in. gasket diameter*)
             Wm1
             (* lb., Must run "Flange stress_hub_ 403.nb " to
               define this variable. Minimum required bolt load, for operating *)
             h_{G} = 0.520 (* in., Must run
               "Flange stress_hub_403.nb" to define this variable.Bending moment length *)
             \sigma_u = 77000.0 \; (*psi, 316 L \; ultimate \; strength*)
             \sigma_{\rm a} = \frac{16700}{K_{\rm b}} (*psi, 316 L allowable strength*)
Out[1257] = 0.3
Out[1258]= 402.5
Out[1259]= 1.
Out[1260] = 8.54
Out[1261]= 24677.2
Out[1262]= 0.52
Out[1263]= 77000.
Out[1264]= 7330.99
In[1265]:= t_{h} = d_{ga} \sqrt{\frac{(C_{a} * p)}{(\sigma_{a} * E_{f})}} + \frac{(1.9 * W_{m1} * h_{g})}{(\sigma_{a} * E_{f} * d_{ga}^{3})}  (* in., required flange thickness *)
Out[1265] = 1.26123
```

 $In[1266] := If[t_h < 1.5, "flange thickness is OK", "flange thickness is NOT OK"]$ Out[1266] = flange thickness is OK

. . In[1565]:= (* Maximum distance between

```
hole centers for a cluster of holes in head, UG-36 (3) (d)*)

(* No two unreinforced openings shall have their centers closer than: *)

R

d_{batweenholes1} = Sin \left[ 36 \times \frac{\pi}{180} \right] \times R \times 2

d_2 = 0.625

d_1 = d_2 (* diameter of holes *)

C_d = 2.5 (d_1 + d_2)

If [d_{betweenholes1} > C_d,

"distance between 5.5 BC holes OK", "distance between 5.5 BC holes NOT OK"]

d_{betweenholes2} = R - .75 - .3125

d_2 = 0.625

d_1 = 1.500

C_d = 2.5 (d_1 + d_2)
```

If[d_{batweenholes2} > C_d, "distance between center hole and 5.5 BC holes OK", "distance between center hole and 5.5 BC holes NOT OK,,,, use alternative UG-39(d)"]

$$\begin{split} & d_{\text{betweenholes2}} < 2 \left(\frac{(d_1 + d_2)}{2} \right) \\ & d_{\text{betweenholes2}} > 1.25 \left(\frac{(d_1 + d_2)}{2} \right) \end{split}$$

(* in., required flange thickness, UG-39 (e) (1) (2), using alternative to Area reinforcment of UG39 (b) (1) *)

$$\sigma_a = 16700$$

$$ef = \frac{R - (\frac{(d_1 \cdot d_2)}{2})}{R} (* UG39 (e) (2) *)$$

$$fs = \sqrt{0.5 / ef}$$

$$t_h = d_{ga} \sqrt{fs \times 2 \left(\frac{(C_a * p)}{(\sigma_a * E_f)} + \frac{(1.9 * W_{m1} * h_G)}{(\sigma_a * E_f * d_{ga}^3)}\right)}$$

Out[1565]= 2.75

Out[1566]= 3.23282
Out[1567]= 0.625
Out[1568]= 0.625
Out[1569]= 3.125
Out[1570]= distance between 5.5 BC holes OK
Out[1571]= 1.6875

. .

Out[1572] = 0.625

Out[1573]= 1.5

Out[1574] = 5.3125

Out[1575]= distance between center hole and 5.5 BC holes NOT OK, , , , use alternative UG-39(d)

Out[1576]= True

- *Out[1577]=* True
- Out[1578] = 16700
- Out[1579] = 0.613636
- Out[1580]= 0.902671

Out[1581]= 1.12279

. . . 10 Out[1589]= 0.625

Out[1590]= 1.5

Out[1591]= 5.3125

Out[1592] = distance between center hole and 5.5 BC holes NOT OK, , , , use alternative UG-39(d)

Out[1593]= True

- *Out[1594]=* True
- Out[1595] = 16700
- Out[1596] = 0.613636
- Out[1597] = 0.902671

Out[1598] = 1.24385

```
(*must run "Flange stress_hub_978.nb"
  file first to save variables defined below into memory*)
(* Assumptions: Chamber head design has has no holes *)
Ro = 5.25 (*in., Flange outside radius*)
C_{0} = 0.3
           (*flange attachment constant*)
p = 850 × 1.15 (*psi, MAWP*)
E_{f} = 1.0
          (*Efficiency Factor *)
d<sub>ga</sub> = G (*in. gasket diameter*)
Wm1
(* lb., Must run "Flange stress_hub_ 978.nb
  " to define this variable. Minimum required bolt load, for operating *)
h_{G} = 0.520 (* in.,
Must run "Flange stress_hub_978.nb" to define this variable.Bending moment length *)
\sigma_u = 77000.0 (*psi, 316 L ultimate strength*)
\sigma_a = 16700 (*psi, 316 L allowable strength*)
0.3
977.5
1.
7.98
58849.9
0.52
77000.
16700
t_{h} = d_{ga} \sqrt{\frac{(C_{e} \star p)}{(\sigma_{a} \star E_{f})} + \frac{(1.9 \star W_{m1} \star h_{G})}{(\sigma_{a} \star E_{f} \star d_{ya}^{3})}} \quad (* \text{ in., required flange thickness } \star)
1.2468
If [t_h < 1.980, "flange thickness is OK", "flange thickness is NOT OK"]
flange thickness is OK
(* Minimum thickness of plate under gasket (hub) *)
tg = d_{ga} \sqrt{(1.9 * W_{m1} * h_G) / (\sigma_a * d_{ga}^3)} (* UG34, sketch (k) *)
```

If[tg < 1.980, "flange hub thickness is OK", "flange hub thickness is NOT OK"]
0.660529</pre>

flange hub thickness is OK

. .

```
(*must run "Flange stress_hub_small_978.nb"
  file first to save variables defined below into memory*)
(* Assumptions: Head design has has no holes *)
Ro = 4.63/2 (*in.,Flange outside radius*)
C_{0} = 0.3
          (*flange attachment constant*)
p = 850 \times 1.15 (*psi, MAWP*)
E_{f} = 1.0
          (*Efficiency Factor *)
d<sub>ga</sub> = G (*in. gasket diameter*)
Wm1
(* 1b., Must run "Flange stress_hub_small_978.nb
  " to define this variable. Minimum required bolt load, for operating *)
h_{g} = 0.520 (* in., Must run
  "Flange stress_hub_small_978.nb" to define this variable.Bending moment length *)
\sigma_{\rm a} = 16700 (*psi, 304 L allowable strength*)
0.3
977.5
1.
3.35
10143.7
0.52
16700
t_{h} = d_{ga} \sqrt{\frac{(C_{o} * p)}{(\sigma_{a} * E_{f})}} + \frac{(1.9 * W_{m1} * h_{G})}{(\sigma_{a} * E_{f} * d_{ga}^{3})}} (* \text{ in., required flange thickness } *)
0.613356
If [t_h < 0.750, "flange thickness is OK", "flange thickness is NOT OK"]
flange thickness is OK
```

(* Minimum thickness of plate under gasket (hub) *)

 $tg = d_{ga} \sqrt{(1.9 * W_{m1} * h_G) / (\sigma_a * d_{ga}^3)} (* UG34, sketch (k) *)$

If[tg < 0.81, "flange hub thickness is OK", "flange hub thickness is NOT OK"]
0.423249</pre>

flange hub thickness is OK

Ś



(5)

(* Bolted Flange Connections with flat metal Copper Gasket, Xe chamber high voltage feedthru *) (* 350 psia MOP, conflat type head *)

(* Bolt Load at operating conditions *) G = 0.72 (* Diameter, in. at gasket load location *) P = 350 * 1.15 (* MAWP, internal design pressure *) m = 4.75 (* gasket factor flat Cu gasket, Table 2-4.1 *) $N_g = 0.25$ (* width of Cu gasket *) $b_o = \frac{N_g}{32}$ (* N/4 for multiple servations Table 2-5.2 (5), assume N/32 given a single knife edge serration as used in Conflats *) $If[b_o \le 0.25, b = b_o, b = .5\sqrt{b_o}]$ y = 13000 (* psi, design seating stress for soft copper, Table 2-5.1 *) $H = 0.785 G^2 P$ (* lb., Total hydrostatic end force *) $H_p = 2b \times \pi GmP$ (* lb., Total joint-contact surface compression load *) $W_{m1} = H + H_p$ (* Minimum required bolt load, for operating *) $W_{m2} = \pi G by$ (* Minimum required bolt load, for gasket seating *) 0.72 402.5 4.75 0.25 0.0078125 0.0078125 13000 163.795 67.5712 231.366 229.729

```
In[54]:= (* Design Bolt Load*)
          A_b = \frac{\pi \times 0.1248^2}{4} \times 6 \; (* cross \; sectional \; area \; of \; \#8-32 \; screw*)
          SF = 4 (* MEDSS *)
          S_{T} = 81000
          (*Unbrako - KS 1216 8-32 SHCS, 160, ksi tensile strength; T = -400 °F to 1200 °F
          OR ASTM-A493-95 Grade S30430; 81 ksi tensile strength *)
          S_a = S_T \div SF
          L_b = S_a \times A_b (* lb., Max allowable bolt load *)
          A_{m1} = W_{m1} / S_a (* in<sup>2</sup>, cross-sectional area of bolts under operating condition *)
          A_{m2} = W_{m2} / S_a (* in^2, cross-sectional area of bolts for gasket seating *)
          If[A_{m1} > A_{m2}, A_m = A_{m1}, A_m = A_{m2}]
          (* in<sup>2</sup>, total required cross-sectional area of bolts *)
          W_o = W_{m1} (* lb., Flange design bolt load, for operating *)
          W_{g} = \frac{(A_{m} + A_{b}) S_{a}}{2} (* lb., Flange design bolt load, for gasket seating *)
          SF_u = L_b SF / W_g
Out[54]= 0.0733956
Out[55] = 4
Out[56]= 81.000
Out[57]= 20250
Out[58]= 1486.26
Out[59]= 0.0114255
Out[60]= 0.0113446
Out[61]= 0.0114255
Out[62]= 231.366
Out[63]= 858.814
Out[64]= 6.92239
```

. ۱

```
C<sub>e</sub> = 0.3 (*flange attachment constant*)
p = 350 × 1.15 (*psi, MAWP*)
E<sub>f</sub> = 1.0 (*Efficiency Factor *)
d<sub>ga</sub> = G (*in. gasket diameter*)
Wm1
(* 1b., Minimum required bolt load, for operating *)
h<sub>G</sub> = 0.171 (* in., Bending moment length *)
\sigma_u = 77000.0 \; (*psi, 304 L ultimate strength*)
\sigma_a = 16700 (*psi, 304 L allowable strength*)
t_{h} = d_{ga} \sqrt{\frac{(C_{o} * p)}{(\sigma_{a} * E_{f})}} + \frac{(1.9 * W_{m1} * h_{G})}{(\sigma_{a} * E_{f} * d_{ga}^{3})} \quad (* \text{ in., required flange thickness }*)
0.3
402.5
1.
0.72
231.366
0.171
77000.
16700
0.1
```



(5)

(* Bolted Flange Connections with flat metal Copper Gasket, Xe chamber gamma ray feedthru *) (* 350 psia MOP, conflat type head *)

(* Bolt Load at operating conditions *) G = 1.650 (* Diameter, in. at gasket load location *) P = 350 * 1.15 (* MAWP, internal design pressure *) m = 4.75 (* gasket factor flat Cu gasket, Table 2-4.1 *) $N_g = 0.25$ (* width of Cu gasket *) $b_o = \frac{N_g}{32}$ (* N/4 for multiple servations Table 2-5.2 (5), assume N/32 given a single knife edge serration as used in Conflats *) $If[b_o <= 0.25, b = b_o, b = .5\sqrt{b_o}]$ y = 13000 (* psi, design seating stress for soft copper, Table 2-5.1 *) $H=0.785\;G^2\;P\;(\star$ 1b., Total hydrostatic end force $\star)$ $H_p = 2b \times \pi GmP$ (* 1b., Total joint-contact surface compression load *) $W_{m1} = H + H_p$ (* Minimum required bolt load, for operating *) $W_{m2} = \pi G b y$ (* Minimum required bolt load, for gasket seating *) 1.65 402.5 4.75 0.25 0.0078125 0.0078125 13000 860.208 154.851 1015.06 526.462

. .

```
In[76]:= (* Design Bolt Load*)
          \mathbf{A}_{b} = \frac{\pi \times 0.2052^{2}}{4} \times 6 \; (* \text{cross sectional area of 1/4-28 screw*})
          SF = 4 (* MEDSS *)
          S_{T} = 81000
          (*Unbrako - KS 1216 1/4-28 SHCS, 160, ksi tensile strength; T = -400 °F to 1200 °F
          OR ASTM-A493-95 Grade S30430; 81 ksi tensile strength *)
          S_a = S_T \div SF
          L_b = S_a \times A_b (* lb., Max allowable bolt load *)
          A_{m1} = W_{m1} / S_a (* in<sup>2</sup>, cross-sectional area of bolts under operating condition *)
          A_{m2} = W_{m2} / S_a (* in<sup>2</sup>, cross-sectional area of bolts for gasket seating *)
          If [A_{m1} > A_{m2}, A_m = A_{m1}, A_m = A_{m2}]
          (* in<sup>2</sup>, total required cross-sectional area of bolts *)
          W_o = W_{m1} (* lb., Flange design bolt load, for operating *)
          W_g = \frac{(A_m + A_b) S_a}{2} (* 1b., Flange design bolt load, for gasket seating *)
          SF_u = L_b SF / W_g
Out[76]= 0.198425
Out[77]= 4
Out[78]= 81000
Out[79] = 20250
Out[80]= 4018.1
Out[81]= 0.0501264
Out[82]= 0.0259981
Out[83]= 0.0501264
Out[84]= 1015.06
Out[85]= 2516.58
Out[86]= 6.38661
```

 $C_{e} = 0.13 \quad (*flange attachment constant*)$ $p = 350 \times 1.15 \quad (*psi, MAWP*)$ $E_{f} = 1.0 \quad (*Efficiency Factor *)$ $d_{ga} = G \quad (*in. gasket diameter*)$ $W_{m1} \quad (* lb., Minimum required bolt load, for operating *)$ $h_{G} = 0.331 (* in., Bending moment length *)$ $\sigma_{u} = 77000.0 (*psi, 304 L ultimate strength*)$ $\sigma_{a} = 16700 \quad (*psi, 304 L allowable strength*)$ $th = d_{ga} \sqrt{\frac{C_{e} \times p}{\sigma_{a} \times E_{f}}} \quad (* in., required flange thickness, no bending moment *)$

$$t_{ho} = d_{ga} \sqrt{\frac{(C_a * p)}{(\sigma_a * E_f)}} + \frac{(1.9 * W_{m1} * h_g)}{(\sigma_a * E_f * d_{ga}^3)} \quad (* \text{ in., required flange thickness }*)$$

$$t_{hg} = d_{ga} \sqrt{\frac{(C_a * p)}{(\sigma_a * E_f)}} + \frac{(1.9 * W_{m2} * h_g)}{(\sigma_a * E_f * d_{ga}^3)} \quad (* \text{ in., required flange thickness }*)$$

0.13

402.5

1.

1.65

1015.06

0.331

77000.

16700

0.0923592

0.178038

0

526.462

0.109616

```
(* Miscellaneous Calculations *)
 (* UG-36 Openings in Pressure vessels*)
 (* UG-36 (c) (3) (d), No two unreinforced openings shall have their centers
   closer than the sum of their diameters: *)
 (* This applies to all holes in the shell of the vessel. Actual holes have
   reinforcement built into the design so this is concervative. *)
 d_1 = 2.87
 d_2 = 0.5
 \mathbf{l}_{\mathbf{s}} = \mathbf{d}_{1} + \mathbf{d}_{2}
 1 = \frac{\pi \times 7.625}{4} \quad (* \text{ distance between holes*})
 1 >= 1_s
 2.87
 0.5
 3.37
5.98866
 True
 (* Drilled holes not penetrating shell *)
 (* holes must be less than 2 " dia. & not less than 0.25 "\ast)
 D_{i} = 7.625
 t = 0.5
 D_1 / t
 D_i / t >= 10
 7.625
 0.5
 15.25
 True
 d_h = 0.375 (* UNF 3/8-16, major dia. *)
 d_h / D_i
 0.375
 0.0491803
```

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```
Rt = 0.375 (* from graph *)
 If [d_h / D_i < 0.03, Rt = .25, Rt = Rt ]
 t<sub>mn</sub> = t (Rt) (* Appx. 30 Fig. 30-1, remaining wall thickness*)
 0.375
 0.375
                D.5-,1875= 0.313 IN.
 0.1875
d_h = 0.250 (* UNF 1/4-20, major dia. *)
d_h / D_i
 0.25
 0.0327869
Rt = 0.256 (* from graph *)
If [d_h / D_i < 0.03, Rt = .25, Rt = Rt ]
t<sub>mn</sub> = t (Rt) (* Appx. 30 Fig. 30-1, remaining wall thickness*)
 0.256
 0.256
              0.5-0.128 = 0.372 IN.
 0.128
 (* Drilled / tapped holes in unstayed flat head *)
 (* reinforcement required, replacement of area *)
 (* 8-32 for mini conflats *)
tr = 1.26123 (* in., minimum required flange thickness *)
ta = 1.5 (* in., actual flange thickness *)
d_h = 0.164 (* in., hole diameter *)
 d_d = 0.312 (* in., depth of hole *)
Ar = d_h \times d_d (* in.^2, area required *)
Aa = d_h (ta - d_d) (* in.^2, area available *)
If [Aa > Ar, "Reinforcement OK for mini-conflat blind holes",
 "Reinforcement NOT OK for mini-conflat blind holes"]
1.26123
1.5
 0.164
 0.312
0.051168
0.194832
Reinforcement OK for mini-conflat blind holes
```

. .

```
(* Drilled / tapped holes in unstayed flat head *)
 (* reinforcement required, replacement of area *)
 (* 8-32 for mounting brackets inside vessel *)
 tr = 1.26123 (* in., minimum required flange thickness *)
 ta = 1.5 (* in., actual flange thickness *)
 d_h = 0.164 (* in., hole diameter *)
 d_d = 0.25 (* in., depth of hole *)
 Ar = d_h \times d_d (* in.*2, area required *)
 Aa = d_h (ta - d_d) (* in.^2, area available *)
 If [Aa > Ar, "Reinforcement OK for mounting bracket blind holes",
  "Reinforcement NOT OK for mounting bracket blind holes" ]
 1.26123
 1.5
 0.164
 0.25
0.041
0.205
 Reinforcement OK for mounting bracket blind holes
 (* Drilled / tapped holes in unstayed flat head *)
 (* reinforcement required, replacement of area *)
 (* 1/4-28 for medium conflat, center hole *)
 tr = 1.26123 (* in., minimum required flange thickness *)
 ta = 1.5 (* in., actual flange thickness *)
 d_h = 0.250 (* in., hole diameter *)
 d_d = 0.5 (* in., depth of hole *)
 Ar = d_h \times d_d (* in.^2, area required *)
 Aa = d_h (ta - d_d) (* in.^2, area available *)
 If [Aa > Ar, "Reinforcement OK for medium conflat blind holes",
  "Reinforcement NOT OK for medium conflat blind holes" ]
 1.26123
 1.5
 0.25
 0.5
 0.125
 0.25
```

Reinforcement OK for medium conflat blind holes

```
(* Weld impact testing exemption calculation *)
(* UHA-51 (g) *)
Sa = 16700
S1 = 3499.17
S<sub>vm</sub> = 7754.6879
If [S1/Sa < 0.4, "Impact testing NOT required for weld",
"Impact testing REQUIRED required for weld"]
16700
3499.17
7754.6879
Impact testing NOT required for weld
(* Base material Impact testing exemption *)
(* UHA-51 (d) (1) (a) austenitic chromium-nickel stainless steels: 304, 304 L,
316, 316 L.</pre>
```

```
(* Fracture Critical Components *)
In[91]:= (* The applied stress is: *)
         R_{i} = 3.8125
         R_{o} = 4.3125
         MAWP = 978
         \sigma_a = 16700 (*allowable stress for 316 L SST*)
         \sigma_y = 37000
         R_i = 3.8125
         R_{o} = 4.3125
         t = R_o - R_i
         Ratio = \frac{R_o}{R_i}
         If [1.1 < Ratio < 1.5, medium wall]
         If [Ratio < 1.1, thin wall]
         If [Ratio > 1.5, thick wall]
          (*Circumferential Stress, S2*)
         S_{2} = \frac{MAWP (R_{o}^{2} + R_{i}^{2})}{(R_{o}^{2} - R_{i}^{2})}
Out[91]= 3.8125
Out [92] = 4.3125
Out[93]= 978
Out[94] = 16700
Out[95]= 37000
Out[96]= 3.8125
Out[97]= 4.3125
Out[98] = 0.5
Out[99]= 1.13115
Out[100] = medium wall
Out[103]= 7976.34
        (* First consider actual stress intensity factors from literature (testing). Then
           apply this K_{Ic} = K_I value to the Xe vessel at its MAWP/stress *)
        (* Degraded Piping Program Phase II, 4/99 *)
        (* Material 304 and 316 stainless steel, range: 561 to 13,400 in-lb/in^2,
         Ji used is the lowest measurable value in all tests, parent or welded material *)
```

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 $f_{i,i} \in$

In[14]:= Ji = 561 (* in-lb/in^2 *) v = 0.33 (* Poisson's ratio *) $E_{\rm Y} = \frac{29.7 \times 10^6}{(1 - v^2)} \; (* \; \rm psi \; *)$ $K_{Ic} = \sqrt{Ji \times E_{Y}} (* psi \sqrt{in} *)$ $a_{crs} = \frac{1}{1.21 \pi} \left(\frac{K_{Ic}}{S_2} \right)^2 (* \text{ in., crack critical length, surface flaw } *)$ $a_{cri} = \frac{1}{\pi} \left(\frac{K_{Ic}}{S_2}\right)^2$ (* in., crack critical length, imbedded flaw *) $lengthc_{crs} = 4 \times a_{crs}$ $lengthc_{cri} = 4 \times a_{cri}$ (* considering leak before break criteria, leak occurs occurs before catastrophic failure in a pressure vessel when *) $\sqrt{\frac{\pi t S_2^2}{1 - \frac{1}{2} \left(\frac{S_2}{\sigma_v}\right)^2}} \quad (* \text{ Fracture and Fatigue Control in Structures},$ Rolfe and Barsom, Prentice-Hall, 1977, pg. 394*) $K_{Ic} >= \sqrt{\frac{\pi t S_2^2}{1 - \frac{1}{2} \left(\frac{S_2}{S_c}\right)^2}} \quad (* \text{ Hoop stress applies, } S_2 \ *)$ If $[K_{IC} > = \sqrt{\frac{\pi t S_2^2}{1 - \frac{1}{2} \left(\frac{S_2}{2}\right)^2}}$, "Leaking should occur before failure", "failure may occur before leaking"

(* LIFE Expectancy Cycles *)

 $a_o = 0.125$ (* in., initial flaw size *) A = 3.0×10^{-10} (* Metal Fatigue in Engineering, 1980, John Wiley & Sons, pg 86 *) n = 3.25 (* Metal Fatigue in Engineering, 1980, John Wiley & Sons, pg 86 *)

$$N_{f} = \frac{2}{2 - n} \left(\frac{1}{A \left(1.12 \frac{s_{2}}{1000} \sqrt{\pi} \right)^{n}} \right) \left(a_{ors} \left(\frac{2 - n}{2} \right) - a_{o} \left(\frac{2 - n}{2} \right) \right)'$$

(* Damage Tolerant Design Handbook " V.2, 1983 *)

$$N_{f} = \frac{2}{2 - n} \left(\frac{1}{A \left(1.12 \frac{s_{2}}{1000} \sqrt{\pi} \right)^{n}} \right) \left(a_{cri} \left(\frac{2 - n}{2} \right) - a_{0} \left(\frac{2 - n}{2} \right) \right)$$

(* Damage Tolerant Design Handbook " V.2, 1983 *)

Out[14] = 561

Out[15] = 0.33

. $Out[16] = 3.33296 \times 10^7$

- Out[17] = 136740.
- Out[18]= 77.3126
- Out[19] = 93.5482
- Out[20] = 309.25
- Out[21]= 374.193
- Out[22]= 10115.1
- *Out[23]=* True
- Out[24]= Leaking should occur before failure
- Out[25] = 0.125
- $Out[26] = 3. \times 10^{-10}$
- Out[27]= 3.25
- $Out[28] = 2.42577 \times 10^{6}$
- $Out[29] = 2.43076 \times 10^{6}$

In[60]:= (* For the ellipsoidal head *) $D_i = 7.625$ $t_{w} = 0.5$ $E_f = 0.7$ (*butt weld efficiency based on no inspection, Table UW-12*) $\sigma = \frac{\text{MAWP} (D_i + 0.2 t_w)}{(2 E_f t_w)}$ $S_2 = \sigma$ $a_{crs} = \frac{1}{1.21\pi} \left(\frac{K_{rc}}{S_2}\right)^2 (* \text{ in., crack critical length, surface flaw }*)$ $a_{cri} = \frac{1}{\pi} \left(\frac{K_{Ic}}{S_{2}}\right)^{2}$ (* in., crack critical length, imbedded flaw *) $lengthc_{crs} = 4 \times a_{crs}$ $lengthc_{cri} = 4 \times a_{cri}$ (* considering leak before break criteria, leak occurs occurs before catastrophic failure in a pressure vessel when *) $\sqrt{\frac{\pi t S_2^2}{1 - \frac{1}{2} \left(\frac{S_2}{2}\right)^2}}$ (* Fracture and Fatigue Control in Structures, Rolfe and Barsom, Prentice-Hall, 1977, pg. 394*) $K_{Ic} >= \sqrt{\frac{\pi t S_2^2}{1 - \frac{1}{2} \left(\frac{S_2}{S_c}\right)^2}} (* \text{ Hoop stress applies, } S_2 *)$ $If \left[K_{Ic} > = \sqrt{\frac{\pi t S_2^2}{1 - \frac{1}{2} \left(\frac{S_2}{C_c}\right)^2}},\right]$ "Leaking should occur before failure", "failure may occur before leaking"] (* LIFE Expectancy Cycles *) a_o = 0.125 (* in., initial flaw size *)

A = 3.0×10^{-10} (* Metal Fatigue in Engineering, 1980, John Wiley & Sons, pg 86 *) n = 3.25 (* Metal Fatigue in Engineering, 1980, John Wiley & Sons, pg 86 *)

$$N_{f} = \frac{2}{2-n} \left(\frac{1}{A \left(1.12 \frac{s_{2}}{1000} \sqrt{\pi} \right)^{n}} \right) \left(a_{ors} \left(\frac{2-n}{2} \right) - a_{o} \left(\frac{2-n}{2} \right) \right)$$

(* Damage Tolerant Design Handbook " V.2, 1983 *)

$$N_{f} = \frac{2}{2 - n} \left(\frac{1}{A \left(1.12 \frac{s_{2}}{1000} \sqrt{\pi} \right)^{n}} \right) \left(a_{cri} \left(\frac{2 - n}{2} \right) - a_{o} \left(\frac{2 - n}{2} \right) \right)$$

(* Damage Tolerant Design Handbook " V.2, 1983 *)

Out[60]= 7.625

Out[61]= 0.5

Out[62] = 0.7

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Out[63]= 10792.9

Out[64]= 10792.9

- Out[65]= 42.2259
- Out[66]= 51.0934
- Out[67]= 168.904
- Out[68] = 204.373
- Out[69] = 13824.2
- Out[70]= True
- Out[71]= Leaking should occur before failure
- Out[72] = 0.125
- $Out[73] = 3. \times 10^{-10}$
- Out[74]= 3.25
- Out[75]= 900192.
- Out[76]= 902921.

In[104]:= (* For the flat head *)

 $\sigma = 5182.85 \quad (* \text{ from head} 350 _K_openings2.nb*)$ $S_2 = \sigma$ $a_{crs} = \frac{1}{1.21 \pi} \left(\frac{K_{Ic}}{S_2}\right)^2 \quad (* \text{ in., crack critical length, surface flaw }*)$ $a_{cri} = \frac{1}{\pi} \left(\frac{K_{Ic}}{S_2}\right)^2 \quad (* \text{ in., crack critical length, imbedded flaw }*)$ $lengthc_{crs} = 4 \times a_{crs}$ $lengthc_{cri} = 4 \times a_{cri}$

(* considering leak before break criteria,

leak occurs occurs before catastrophic failure in a pressure vessel when *)

$$\sqrt{\frac{\pi t S_2^2}{1 - \frac{1}{2} \left(\frac{S_2}{\sigma_y}\right)^2}} \quad (* \text{ Fracture and Fatigue Control in Structures},$$

Rolfe and Barsom, Prentice-Hall, 1977, pg. 394*)

$$\begin{split} \mathbf{K}_{\mathrm{Ic}} & \geq = \sqrt{\frac{\pi \mathrm{t} \mathrm{S}_{2}^{2}}{1 - \frac{1}{2} \left(\frac{\mathrm{S}_{2}}{\mathrm{\sigma}_{y}}\right)^{2}}} \quad (* \text{ Hoop stress applies, } \mathrm{S}_{2} \; *) \\ \mathrm{If} \left[\mathrm{K}_{\mathrm{Ic}} & \geq = \sqrt{\frac{\pi \mathrm{t} \mathrm{S}_{2}^{2}}{1 - \frac{1}{2} \left(\frac{\mathrm{S}_{2}}{\mathrm{\sigma}_{y}}\right)^{2}}} \;, \end{split}$$

"Leaking should occur before failure", "failure may occur before leaking"]

(* LIFE Expectancy Cycles *)

 $a_o = 0.125$ (* in., initial flaw size *) A = 3.0×10^{-10} (* Metal Fatigue in Engineering, 1980, John Wiley & Sons, pg 86 *) n = 3.25 (* Metal Fatigue in Engineering, 1980, John Wiley & Sons, pg 86 *)

$$N_{f} = \frac{2}{2 - n} \left(\frac{1}{A \left(1.12 \frac{s_{2}}{1000} \sqrt{\pi} \right)^{n}} \right) \left(a_{crs} \left(\frac{2 - n}{2} \right) - a_{c} \left(\frac{2 - n}{2} \right) \right)$$

(* Damage Tolerant Design Handbook " V.2, 1983 *)

$$N_{f} = \frac{2}{2 - n} \left(\frac{1}{A \left(1.12 \frac{s_{2}}{1000} \sqrt{\pi} \right)^{n}} \right) \left(a_{cri} \left(\frac{2 - n}{2} \right) - a_{0} \left(\frac{2 - n}{2} \right) \right)$$

(* Damage Tolerant Design Handbook " V.2, 1983 *)

- Out[104]= 5182.85
- Out[105]= 5182.85
- Out[106] = 183.113
- Out[107] = 221.567

Out[108]= 732.454

Out[109]= 886.269

Out[110]= 6527.84
Out[111]= True
Out[112]= Leaking should occur before failure
Out[113]= 0.125
Out[114]= 3.×10⁻¹⁰
Out[115]= 3.25

 $Out[116] = 9.92359 \times 10^{6}$

 $Out[117] = 9.93542 \times 10^{6}$

- (* Fragment Evaluation *)
- (* It is assumed that the most vulnerable point in this vessel is the Ceramaseal high voltage feedthroughs mounted to the mini-Conflats which are mounted to the 350 MOP head. These could easily be bumped or damaged by mishandling resulting in a fragment / projectile. The following will estimate the shielding thickness required for personnel protection near the vessel head. Also assume all of the energy is transferred to a single fragment. *)

$$In[22] := m_{fg} = 37.7 \ (* g; actual measurment *)$$
$$m_{fs} = m_{fg} * 6.852 \times 10^{-5} \ (* lb.s^2/ft; slugs *)$$
$$v_{f} = \sqrt{\frac{2 \text{ Energy}}{m_{fs}}} \ (* ft/s *)$$

Out[22]= 37.7

- Out[23] = 0.0025832
- Out[24]= 6575.9

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$$\begin{split} P_{ratio} &= \frac{P_1}{P_2} (* *) \\ g &= 32.2 (* ft/s^2 *) \\ T &= 528 (* {}^{\circ}R *) \\ k &= 1.4 \\ R &= 53.3 (* ft-lb/lb-{}^{\circ}R *) \\ a &= \sqrt{kgRT} \\ v_{f1} &= a \times 2.55 (* ft/s \ Figure 12 \ Zero \ Mass \ velocity *) \\ v_{f12} &= v_{f1} \ Cos \Big[\frac{0.785398}{2} \Big] (* \ MEDSS \ eqn. \ 38 *) \\ v_{f1m} &= v_{f1} \times 0.3048 (* m/s *) \\ v_{f1m2} &= v_{rf} \times 0.3048 (* m/s *) \\ m_1 &= \frac{2 \ Energy}{v_{f1}^2} \ 32.2 (* \ lb_m; \ largest \ fragment \ that \ can \ achieve \ this \ velocity *) \\ Out[95] &= \ 32.2 \end{split}$$

Out[96]= 528

Out[97]= 1.4

Out[98]= 53.3

Out[99]= 1126.35

Out[100]= 2872.19

Out[101]= 2653.55

Out[102]= 875.443

Out[103] = 808.804

Out[104] = 0.436013

(* The Ceramaseal feedthrough mass is < m1 so it can only achive this maximum velocity.

Fragment shielding evaluation..... *)

. .

```
In[105] := T_{m} = 6 \times 10^{-5} \left(\frac{m_{fg}}{1000}\right)^{0.33} v_{flm} (* \text{ UK formula }*)T_{m} = T_{m} \times 12 \times 3.28084 (* \text{ in }*)(* \text{ Thor formula: Lexan }*)\alpha = 1.814\beta = -1.652c_{1} = 7.329A_{f} = \frac{\pi \ 0.5^{2}}{4}T_{in} = \frac{1}{A_{f}} \left(\frac{v_{fl}}{10^{c_{1}} (7000 \frac{m_{1}}{32.2})^{\beta}}\right)^{\frac{1}{n}}
```

Out[105]= 0.0178062

Out[106] = 0.701032

Out[107]= 1.814

Out[108] = -1.652

Out[109] = 7.329

Out[110]= 0.19635

Out[111] = 2.36231

(* After ricochet the shielding thickness needs to be:*)

.

```
\begin{split} \mathbf{T}_{m} &= 6 \times 10^{-5} \left(\frac{\mathbf{m}_{fg}}{1000}\right)^{0.33} \mathbf{v}_{flm2} \; (* \; m; \; \text{UK formula } *) \\ \mathbf{T}_{m} &= \mathbf{T}_{m} \times 12 \times 3.28084 \; (* \; \text{in } *) \\ &(* \; \text{Thor formula: Lexan } *) \\ &\alpha &= 1.814 \\ &\beta &= -1.652 \\ &\mathbf{c}_{1} &= 7.329 \\ &\mathbf{A}_{f} &= \frac{\pi \; 0.5^{2}}{4} \\ &\mathbf{T}_{in} &= \frac{1}{\mathbf{A}_{f}} \left(\frac{\mathbf{v}_{f12}}{10^{c_{1}} \; (7000 \; \frac{\mathbf{m}_{i}}{32.2})^{\beta}}\right)^{\frac{1}{\alpha}} \end{split}
```

Out[112]= 0.0164508

Out[113] = 0.647669

Out[114]= 1.814

Out[115] = -1.652

Out[116]= 7.329

Out[117] = 0.19635

Out[118] = 2.26142

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