

Note: under EN_13455-3 rules for 316Ti, a thinner thickness of 10.25 mm is possible, due to a higher maximum allowable strength at the knuckle. Below is an analysis from Sara Carcel

| Torispherical heads, VIII, Div 2 | | | DIN 28011 | | EN 13445-3 (316Ti, para D | |
|----------------------------------|------------|-----------|------------|--------------------------|---------------------------|-------------------|
| | KORBBOGEN | | r=0,1L | | f | 166.666667 |
| D | 1360 | | 1360 | Diámetro interior | X | 0.1 |
| t | 10 | | 10 | | t | 10 |
| De | 1380 | | 1380 | | Y | 0.00735294 |
| L | 1104 | | 1360 | Diámetro interior corona | Z | 2.13353891 |
| ri | 212.52 | | 136 | | N | 0.84954918 |
| L/D | 0.81176471 | Ok | 1 | Entre 0,7 y 1, ver 4-49 | $\beta_{0,1}$ | 0.86799204 |
| ri/D | 0.15626471 | Ok | 0.1 | Mayor de 0,06 | $\beta_{0,2}$ | 0.51421113 |
| Li/t | 110.4 | Ok | 136 | Entre 20 y 2000 | β | 0.86799204 |
| β | 1.01880199 | | 1.11024234 | | P | 1.52 |
| φ | 0.49440713 | | 0.85749293 | | eb | 8.66383993 |
| R | 752.567792 | | 697.850818 | Si $\varphi < \beta$ | ey | 10.2275849 |
| C1 | 0.71313518 | r/D>0,08 | 0.6742 | | es | 6.21577196 |
| C2 | 1.05371176 | | 1.2 | | Thickness | 10.2275849 |
| Peth | 64.2498476 | E=117000 | 44.2387943 | | | |
| C3 | 206 | Sy=206MPa | 206 | | | |
| Py | 3.37117586 | | 1.57121205 | | | |
| G | 19.0585868 | | 28.1558395 | | | |
| Pck | 6.73919067 | | 3.14731728 | G>1 | | |

Nozzle wall thickness required

Internal radius of finished opening

$$R_n := 4.4\text{cm}$$

Thickness required for internal pressure:

$$t_m := \frac{P \cdot R_n}{S \cdot E - 0.6 \cdot P} \quad t_m = 0.501\text{ mm}$$

We set nozzle thickness

$t_n := 7\text{mm}$ we are limited by need to maintain CF bolt pattern which has typically a 4.0 inch OD pipe with room for outside fillet weld

$$D_{on} := 2(R_n + t_n) \quad D_{on} = 4.016\text{in}$$

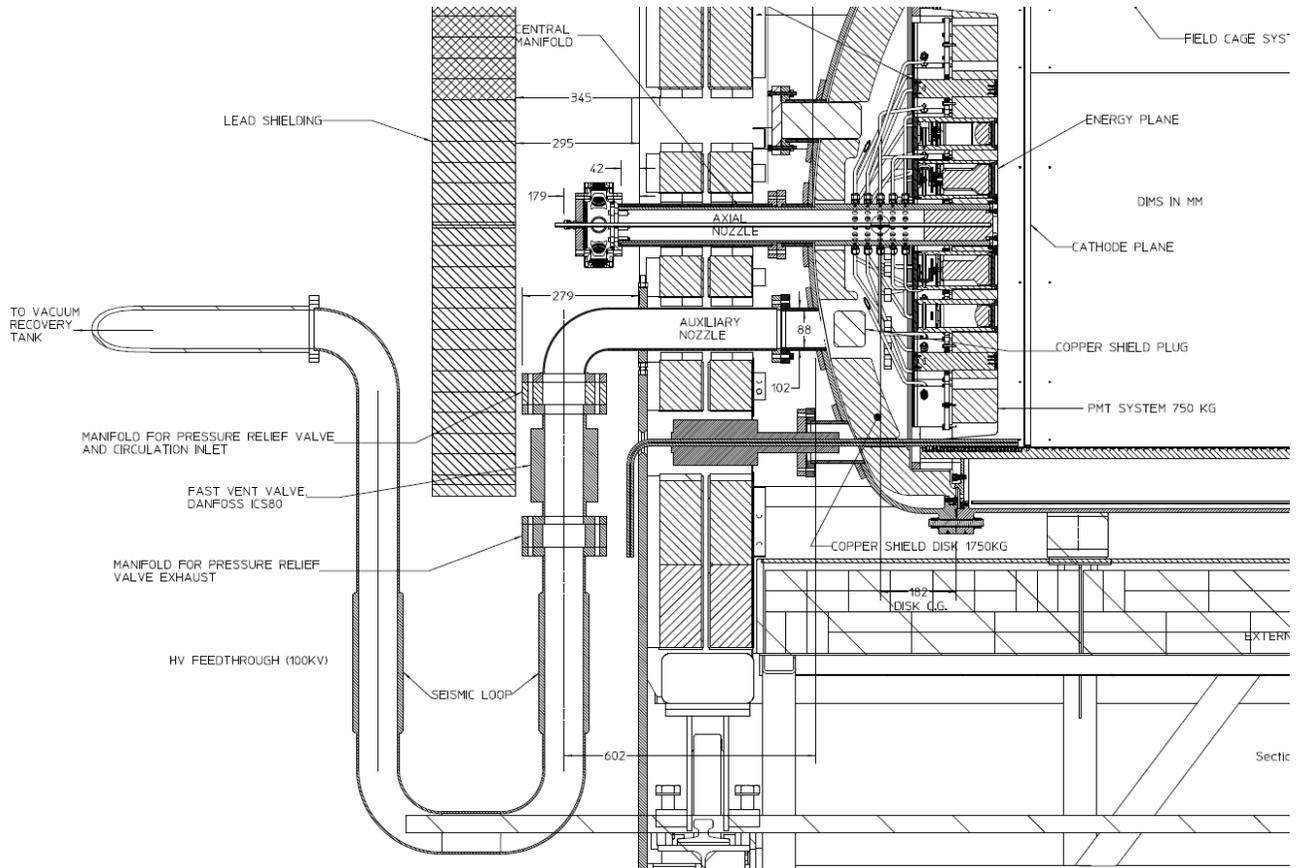
Thickness required for external loading

Nozzles on head may be subject to several possible non-pressure loads, simultaneously:

1. Reaction force from pressure relief, (fire) or fast depressure (auxiliary nozzle only)
2. Weight of attached components, including valves, expansion joints, high voltage feedthrough.

The nozzles may all have nozzle extensions rigidly attached which create to possibility of high moments being applied to the nozzles, not just shear loads. We consider the direction and location of center of gravity for these loads.

Current plan to use a straight through solenoid valve, Danfoss ICS80, aimed downward, to minimize shielding plug width. A seismic loop will be plumbed in so as to make reaction force in line with the vessel nozzle, under steady state vent conditions. However, a transient force will be present until the vent pipe fills, so we plan for this reaction force, which will be vertically upward, counteracting weight of valve and other components on the nozzle extension.



D. Shuman
rev. A July 29, 2012 using 15 kg/s vent rate
and current vent line with seismic loop

Component masses:

from CAD mass measurements 7/27/12

| | | | | | |
|-------------------|-----------------|--------------|----------------|------------------------|---------------------------------|
| pres relief valve | fast vent valve | flange, each | manifold, each | seismic loop w/flanges | nozzle extension pipe and elbow |
|-------------------|-----------------|--------------|----------------|------------------------|---------------------------------|

$$m_{prv} := 2\text{kg} \quad m_{fvv} := 15\text{kg} \quad m_{fl} := 5\text{kg} \quad m_{manifold} := 10\text{kg} \quad m_{seis_loop} := 70\text{kg} \quad m_{pipe} := 4\text{kg}$$

total mass of vent line supported by nozzle

$$m_{vent_line} := m_{pipe} + 3 \cdot m_{fl} + m_{fvv} + m_{prv} + 2m_{manifold} + 0.5 \cdot m_{seis_loop}$$

$$m_{vent_line} = 91\text{kg}$$

distance horizontal, from nozzle-head junction to valve and vessel half of seismic loop (other end of seismic loop supported by work platform)

$$l_{valve} := 60\text{cm}$$

Vent rate, Danfoss ICS80 valve and associated vent piping, as calculated elsewhere

$$15 \frac{\text{kg}}{\text{s}} = 1.19 \times 10^5 \frac{\text{lb}}{\text{hr}}$$

Fast vent reaction force, as calculated below, from Anderson Greenwood Technical Seminar Manual, pg 49

6.3.1 Reactive Force for GASES

On larger orifice, higher pressure valves, the reactive forces during valve relief can be substantial. External bracing might be required. Refer to Figure 6-7.

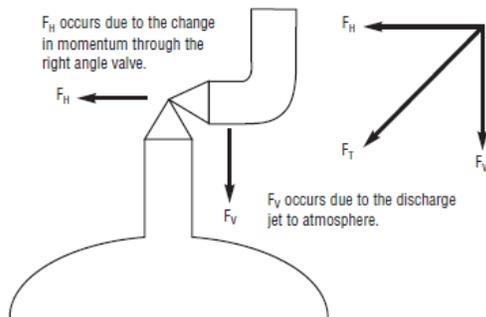


Figure 6-7. Reactive Force

API RP 520, Part 2 gives the following formula for calculating this force.

$$F_T = \frac{W \sqrt{\frac{kT}{(k+1)M}}}{366} + (A_o \times P_2) = F_H + F_V \quad (1)$$

Where:

- F_T = Reactive force at the point of discharge to the atmosphere (lbs.)
- W = Flow of any gas or vapor (lb./hr.)
- k = Ratio of specific heats (C_p/C_v)
- T = Inlet temperature, absolute ($^{\circ}\text{F} + 460$)
- M = Molecular weight of flowing media
- A_o = Area of the outlet at the point of discharge (in^2)
- P_2 = Static pressure at the point of discharge (psig)

$$F_H := \frac{W \cdot \sqrt{\frac{k \cdot T}{(k+1) \cdot M_a}}}{366} \quad F_H := \frac{119000 \cdot \sqrt{\frac{1.67 \cdot 535}{(1.67+1) \cdot 136}}}{366} \cdot \text{lb} \quad F_H = 510 \text{ lbf} \quad F_H = 2.269 \times 10^3 \text{ N}$$

$$A_o := \frac{\pi}{4} 80\text{mm}^2 \quad P_2 := 15\text{bar}$$

$$F_V := A_o \cdot P_2 \quad F_V = 21.5 \text{ lbf} \quad F_V = 95.5 \text{ N}$$

$$F_T := F_H + F_V \quad F_T = 2364 \text{ N}$$

Moments:

$$M_{vent_weight} := -g \cdot l_{valve} \cdot (0.5m_{pipe} + 3 \cdot m_{fl} + m_{fvv} + m_{prv} + 2m_{manifold} + 0.5 \cdot m_{seis_loop})$$